

1 **Life cycle assessment of a carbon capture utilization and storage supply chain in Italy and Germany:**  
2 **comparison between carbon dioxide storage and utilization systems**

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11 **Abstract**

12 The main purpose of this work is to verify that the CCUS supply chains at large scale that were developed in  
13 previous studies for Italy and Germany effectively reduce carbon emissions. The methodology of life cycle  
14 analysis was applied.

15 Results showed that the annual global warming potential (GWP) for the supply chain in Italy and Germany is  
16 respectively of  $9.62 \times 10^{10}$  kgCO<sub>2-eq</sub> and  $1.94 \times 10^{11}$  kgCO<sub>2-eq</sub>, then these Countries will be able to achieve the  
17 carbon dioxide reduction target fixed by the European environmental policies. In fact, overall emissions in  
18 Italy and Germany are 249 Mtonne/year and 640 Mtonne/year, respectively.

19 From the sensitivity analysis, it results that for the supply chain in Germany the GWP increases when, for a  
20 fixed amount of emissions captured, more carbon dioxide is sent to utilization: storage is then important to  
21 achieve the environmental target. Other impact categories decrease, increase or remain constant. On the other  
22 hand, for the supply chain in Italy, results showed that a lower environmental impact can be obtained increasing  
23 the carbon utilization rate for methane production via power to gas system. Then, this utilization system is  
24 more environmentally friendly than the storage option and other utilization processes.

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26 **Keywords:** CCUS supply chain, life cycle assessment analysis, carbon dioxide emissions, sensitivity analysis.

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31 **Abbreviations**

32 ADP, abiotic depletion potential

- 33 AIMMS, advanced interactive multidimensional modeling system
- 34 AP, acidification potential
- 35 CED, cumulative energy demand
- 36 CCU, carbon capture and utilization
- 37 CCUS, carbon capture utilization and storage
- 38 CCS, carbon capture and storage
- 39 EP, eutrophication potential
- 40 FAETP, fresh water aquatic ecotoxicity potential
- 41 GWI, global warming impact
- 42 GWP, global warming potential, equivalent to GWI
- 43 HTP, human toxicity potential
- 44 IGCC, integrated gasification combined cycle
- 45 LCA, life cycle assessment
- 46 LCI, life cycle inventory
- 47 LCIA, life cycle impact assessment
- 48 MAETP, marine aquatic ecotoxicity potential
- 49 MEA, monoethanolamine
- 50 MDEA, methyl diethanolamine
- 51 NGCC, natural gas combined cycle
- 52 ODP, ozone depletion potential
- 53 PC, pulverized coal
- 54 POCP, photochemical ozone creation potential
- 55 TETP, terrestrial ecotoxicity potential

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64 **1. Introduction**

65 Global carbon dioxide concentration in the atmosphere has rapidly increased over the past decades at the rate  
66 of about 2 ppm/year and exceeded 400 ppm in 2016 (Kahn, 2016). In order to limit the rise of the global  
67 average temperature to 2 °C by 2050, the 2030 Climate and Energy Policy Framework proposed a reduction  
68 in carbon dioxide emissions of at least 40% compared to the 1990 level, by 2030 (General Secretariat of the  
69 Council, 2014) and by 80-95% by 2050 (Pacala and Socolow, 2004). To achieve these aims, carbon supply  
70 chains have an important role and are among the research priorities of the Strategic Energy Technologies (SET)  
71 Plan of the European Union (European Commission, 2015 a,b).

72 Carbon capture and storage (CCS) supply chains, carbon capture utilization (CCU) supply chains and carbon  
73 capture utilization and storage (CCUS) supply chains have been proposed, as widely reported in the special  
74 issue of Zhang et al. (2020). In these technologies, carbon dioxide is captured from flue gases and is transported  
75 to a geological or ocean storage site and/or to a utilization site for its valorization with the production of  
76 valuable compounds (Mac Dowell et al., 2017). CCUS systems have the advantage of being a vital and  
77 potentially effective technology able to decrease emissions (Zhang et al., 2020).

**Commentato [GL1]:** Meglio conservare questa frase perché sottolinea i vantaggi della ccus

79  
80 Carbon supply chains require a significant amount of energy for their operation (especially for carbon dioxide  
81 capture and conversion processes) and this causes an additional environmental penalty. It was estimated that  
82 the increase in fuel consumption per kWh for plants that capture 90% of carbon dioxide by using the best  
83 current technologies ranges from 24 to 40% for new supercritical pulverized coal plants, from 11 to 22% for  
84 natural gas combined cycle plants, and from 14 to 25% for coal-fired integrated gasification combined cycle  
85 systems, compared to similar plants without capture and storage systems (IPCC, 2005). Therefore, it is  
86 necessary to know if a specific carbon supply chain is favorable from an overall environmental point of view.  
87 For this purpose, a life cycle assessment (LCA) analysis should be developed. LCA develops a series of is-a  
88 green metrics that considers all inputs and outputs in a process, analyzed over their entire life cycle (von der  
89 Assen et al., 2014a).

**Commentato [BD2]:** Thats how I understand it anyway

**Commentato [GL3R2]:** ok

91 LCA have been conducted for CCS, CCU and CCUS supply chains in the literature. Most A number of LCA  
92 studies about CCS systems are reported in Table 1. An environmental benefit is not always ensured by-for  
93 this kind of supply chain. In Kim et al. (2019), recommends that only 64% of carbon dioxide emitted by a  
94 power plant beis sequestered and stored, while in Petrescu et al. (2017) a reduction for all environmental impact  
95 categories-metrics is not obtained by using a CCS supply chain. However, there are cases where the use of this  
96 framework does allows a reduction of the Global Warming Potential (GWP), however but does result in a  
97 simultaneous increase of other impact categories-metrics (Corsten et al., 2013; Singh et al., 2011a,b; Cuellar-  
98 Franca and Azapagic, 2015b). On the other hand, o Other studies were focused on the evaluation of GWP and  
99 is-a significant reduction was measured-predicted by Volkart et al. (2013), Ni et al. (2011), Koorneef et al.  
100 (2008) and Koore et al. (2010). In these studies, where carbon dioxide is mainly captured from a power plant.

**Commentato [BD4]:** Should this be most? Is it really all?

**Commentato [GL5R4]:** Yes, it is all.

101 Only a few studies have reported ~~the~~ benefits of a CCS framework for all investigated impact ~~categories~~ metrics  
 102 (Pehnt and Henkel, 2009).

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 106 Table 14 Literature studies about LCA of CCS supply chains

| Work                                | CO <sub>2</sub> source              | Capture technology                              | Results - Effects of using a CCS supply chain  |
|-------------------------------------|-------------------------------------|---|--|
| Cuellar-Franca and Azapagic (2015b) | Power plant                         |   | Reduction of GWP by 63-82% per unit of generated electricity but with an increase of acidification and human toxicity            |
| Volkart et al. (2013)               | Fossil power plant and cement plant |   | Reduction of GWP (68-92% in fossil power plant and 39-72% in cement plant)   |
| Pehnt and Henkel (2009)             | Lignite power plant                 | Post and pre combustion and oxy-fuel technology | Reduction of all impact categories in the pre-combustion technology  |
| Singh et al. (2011a)                | Natural gas combined cycle (NGCC)   |   | Reduction of GWP by 64% with an increase of 43% in acidification, 35% in eutrophication and 120-170% in various toxicity impacts |
| Nie et al. (2011)                   | Power plant                         | Post-combustion and oxy-fuel technology         | Reduction of GWP by 78.8% (post-combustion) 80% (oxy-fuel technology)  |
| Koorneef et al. (2008)              | Coal power plant                    |   | Reduction of GHGs up to 243 g/kWh  |
| Koore et al. (2010)                 | Power plant                         |   | Reduction of GWP by 80%  |
| Singh et al. (2011b)                | Power plant                         |   | Reduction of GHGs by 64-78% but with an increase of toxicity   |
| Corsten et al. (2013)               | Fuel technology                     |   | Reduction of GWP but with an increase of eutrophication and acidification  |
| Petrescu et al. (2017)              | Coal power plant                    | MDEA, aqueous ammonia and calcium looping       | No reduction for all impact categories   |
| Kim et al. (2019)                   | Power plant                         | MEA absorption                                  | Sequestration of only 64% of the emitted CO <sub>2</sub>   |

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109 LCA studies about CCU supply chains are shown in Table 2. ~~A~~ also for this kind of framework, an  
 110 environmental benefit is not always ensured. In Passell et al. (2013), carbon dioxide is used to produce diesel  
 111 from microalgae, but a GWP higher than the conventional petroleum based ~~one route is measured~~ predicted. In  
 112 Han and Lee (2013), carbon dioxide is utilized to produce polymers and bio-butanol, ~~although and~~ a significant  
 113 reduction of the environmental burden is ensured only ~~by~~ decreasing the gas-MEA capture ~~facilities~~. However,  
 114 compared to the conventional production route, ~~environmental advantages by of~~ using a CCU supply chain  
 115 are reported in some studies where carbon dioxide is captured to produce dimethylcarbonate (Aresta and  
 116 Galatola, 1999), polyols (Assen and Bardow, 2014a) and for mineral carbonation (Khoo et al., 2021).

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121 Table 22 Literature studies about LCA of CCU supply chains

| Work | CO <sub>2</sub> source | Capture technology | Utilization route | Results – Effects of using a CCU supply chain |
|------|------------------------|--------------------|-------------------|---|
|------|------------------------|--------------------|-------------------|---|

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|                            |                                       |                |                          |   |
|----------------------------|---------------------------------------|----------------|--------------------------|---|
| Passell et al. (2013)      | Electricity generation plant          |                | Diesel from microalgae   | Higher value of GWP (2.9 kgCO <sub>2eq</sub> /1 MJ of combusted fuel) compared to the petroleum diesel (0.12 kgCO <sub>2eq</sub> /1 MJ of combusted fuel) |
| Aresta and Galatola (1999) | Ammonia production plant              | MEA absorption | Dimethyl carbonate       | Reduction of GWP by 4.3 times compared to the conventional route from phosgene (31 vs 132 kgCO <sub>2eq</sub> /kg dimethylcarbonate)                      |
| Khoo et al. (2021)         | Flue gas from a waste-to-energy plant |                | Mineralization           | Reduction of GWP by 115.78 kgCO <sub>2eq</sub> per tonne of CO <sub>2</sub> input   |
| Han and Lee (2013)         | Gas fired and coal fired power plants | MEA absorption | Polymers and bio-butanol | A significant reduction of the environmental impact is obtained by reducing the gas-MEA capture facilities  |
| Assen and Bardow (2014b)   | Lignite power plant                   |                | Polyols for polyurethane | Reduction of GHG by 11-19% and saving of fossil resource by 13-16% compared to the conventional route   |

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124 LCA ~~works about studies on~~ CCUS supply chains are reported in Table 3, ~~where~~ The utilization route is  
 125 mainly ~~related arising from to the~~ carbon dioxide oil recovery technology (CO<sub>2</sub>-EOR). ~~Studies show allowing~~  
 126 a GHG emission reduction ~~of~~ up to 80% (Hertwich et al., 2008). ~~Liu et al. (2020) found that for this framework~~  
 127 ~~2532.63 kg of carbon dioxide, 74.18 kg of sulfur dioxide and 37.38 kg of nitric oxide per metric ton of crude~~  
 128 ~~oil are produced. On the other hand, Jiang et al. (2017) analyzed different carbon dioxide sources finding~~  
 129 ~~emissions of 114.69-121.50 MtCO<sub>2-eq</sub> for the integrated gasification combined cycle (IGCC) plant and 222.95-~~  
 130 ~~236.19 Mt CO<sub>2-eq</sub> for the pulverized coal (PC) plant.~~

131 The attractiveness ~~of the~~ CCUS scheme was reported by Cooney et al. (2015). ~~They showed that,~~ when  
 132 the crude recovery ratio is increased ~~because~~ emissions are reduced, ~~and by~~ Hussain et al. (2013) proposed ~~ing~~  
 133 different solutions for carbon dioxide source and capture. ~~Moreover, + and that~~ this kind of CCUS scheme  
 134 could ~~ensure~~ result in negative emissions (Hornafius and Hornafius, 2015). When compared to ~~the~~  
 135 conventional oil production, a CCUS framework based on CO<sub>2</sub>-EOR can ensure up to 71% of emission  
 136 reduction (Thorne et al., 2020; Azzolina et al., 2017; Abotalib et al., 2016).

137 In addition to the oil recovery process, other utilization options were considered for the environmental analysis  
 138 of ~~a~~ CCUS supply chains. In Yue and You (2015), carbon dioxide was stored and used to produce algae for  
 139 biofuel production obtaining a reduction ~~in~~ emissions ~~of~~ up to 80% ~~when 187 Mgal of diesel is provided.~~  
 140 ~~Another utilization route was investigated in~~ Fernandez-Dacosta et al. (2018). ~~Here studies,~~ the alternative  
 141 production of dimethyl ether and polyol ~~obtaining~~ ensured lower values of GWP and fossil resources depletion.

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**Commentato [BD6]:** A very specific result and not worth bringing out like this unless there is some general lesson.

**Commentato [GL7R6]:** Ok!

**Commentato [BD8]:** Likewise

**Commentato [BD9R8]:**

**Commentato [GL10R8]:** Ok!

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154 Table 33 Literature studies about LCA of CCUS supply chains

| Work                            | CO <sub>2</sub> source  | Capture technology  | Utilization route            | Results – Effect of using a CCUS supply chain   |
|---------------------------------|---|---------------------|------------------------------|---|
| Hertwich et al. (2008)          | Power plant   | MEA absorption      | Oil recovery                 | Reduction of GHGs by 80%  |
| Cooney et al. (2015)            | Natural dome and power plant  |                     | Oil recovery                 | Reduction of emissions only for natural CO <sub>2</sub> when the crude recovery ratio is increased  |
| Hussain et al. (2013)           | Coal integrated gasification combined cycle (IGCC), switchgrass IGCC, livestock manure biogas |                     | Oil recovery                 | Coal and biomass IGCC CO <sub>2</sub> -EOR, as well as natural gas and biogas NGCC CO <sub>2</sub> -EOR, may be attractive alternatives for reducing GHG emissions  |
| Hornafius and Hornafius (2015)  | Corn ethanol fermentation   |                     | Oil recovery                 | Negative emissions are obtained   |
| Azzolina et al. (2017)          | Coal power plant  |                     | Oil recovery                 | Reduction of emissions compared to the conventional method of extraction  |
| Jiang et al. (2017)             | IGCC and pulverized coal (PC) power plant   |                     | Oil recovery                 | CO <sub>2</sub> emissions are 114.69-121.50 Mtonne CO <sub>2-eq</sub> (for IGCC), 222.95-236.19 Mt CO <sub>2-eq</sub> (for PC)  |
| Abotalib et al. (2016)          | Ethanol plant, coal-fired and natural gas fired power plant                                   |                     | Oil recovery                 | Reduction of carbon intensity compared to conventional crude recovery (up to -1.6 tonneCO <sub>2-eq</sub> /bbl for CO <sub>2</sub> from ethanol plant)  |
| Thorne et al. (2020)            | Power plant   | Oxy-fuel technology | Oil recovery                 | Reduction by 71% of emissions compared to the conventional production of oil  |
| Liu et al. (2020)               |   |                     | Oil recovery                 | Emissions of 2532.63 kg of CO <sub>2</sub> , 74.18 kg of SO <sub>2</sub> and 37.38 kg of NOx per metric tonne of crude oil  |
| Yue and You (2015)              | Power plant   |                     | Algae for biofuel production | Reduction by 80% of CO <sub>2</sub> emissions when 187 Mgal of renewable diesel are produced  |
| Fernandez-Dacosta et al. (2018) | Steam methane reforming unit  |                     | Dimethyl ether and polyol    | Reduction of GWP and fossil depletion compared to the conventional production way (0.239 kgCO <sub>2-eq</sub> /FU and 0.131 kg <sub>oil-eq</sub> /FU vs 0.294 kgCO <sub>2-eq</sub> /FU and 0.14 kg <sub>oil-eq</sub> /FU) |

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157 From this above literature survey results shows the importance of conducting an environmental  
 158 analysis of each carbon supply chain to verify the effective reduction of emission notwithstanding the any  
 159 additional energy consumptions. It is important to juxtapose contrast the LCA with the economic analysis.

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161 Moreover, other carbon-dioxide-based products have not been taken into consideration for the LCA of a  
 162 carbon supply chains and a comparison between carbon dioxide storage and new utilization options has not  
 163 been analyzed so far in the literature for a CCUS framework. As an additional point, previous studies did were  
 164 not considering the application of LCA to a CCUS supply chains at large scale (e.g. taking into account a  
 165 supply chain developed for an entire Nation with the respective consumption and production data).

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167 This study will contribute to fill these gaps. In particular, in previous works, we analysed developed a the CCUS  
 168 supply chain for Germany (Leonzio et al., 2019) producing different carbon-dioxide-based products, such as  
 169 methanol, urea, concrete, wheat, polyurethane, calcium carbonate, lignin (see Supplementary Material), and  
 170 for Italy (Leonzio and Zondervan, 2020) producing methane all at national large scale considering (the whole  
 171 national territory was considered). Beyond clear differences between these supply chains, the aim of this  
 172 research is to verify that each one of the systems optimized before is effectively able to reduce carbon dioxide

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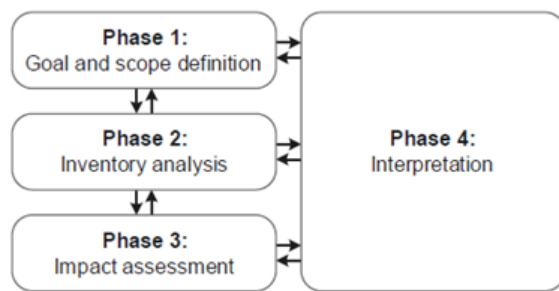
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173 emissions overall according to their respective national environmental targets. In fact, a lot of. A considerable  
174 amount of energy is required for their operation: for the CCUS supply chain of Germany the energy  
175 consumption was of 55.37 GJ/ton CO<sub>2</sub> captured (Leonzio et al., 2019), while for the CCUS supply chain of  
176 Italy the energy consumption was of 28.8 GJ/ton CO<sub>2</sub> captured (Leonzio and Zondervan, 2020).

178 An additional innovative point of this study is the sensitivity analysis developed for both supply chains to  
179 evaluate the influence of aspects of storage and utilization sections on the environmental results. A variable  
180 amount part of the captured carbon dioxide can be sent to the utilization section to produce different  
181 compounds, instead of being stored. This analysis can help the choice between carbon dioxide utilization or  
182 storage in order to create a more environmentally friendly, beneficial system. The paper is divided into two  
183 parts: in the first part, the LCA of the CCUS supply chains in Italy and Germany was developed, while in  
184 the second part the environmental impact was evaluated through the sensitivity analysis, by increasing the  
185 utilization rate of carbon dioxide.

## 186 2. Materials and methods

187 The LCA is a quantitative methodology used to evaluate the environmental impact of systems according to the  
188 standards ISO 14044 and ISO 14040 (ISO 14040, 2009; ISO 14044, 2006). Four important phases characterize  
189 this analysis, as shown in Figure 1: goal and scope, life cycle inventory (LCI) phase, life cycle impact  
190 assessment (LCIA) phase and interpretation phase (von der Assen et al., 2014a; ISO 14040, 2009; ISO 14044,  
191 2006). To develop the LCA, GaBi software with the Ecoinvent database has been used (Education license,  
192 version 6) (Thinkstep, 2019).



196 Figure 1 Stages of a life cycle assessment analysis according to the ISO standards (ISO 14040, 2009; ISO  
197 14044, 2006)

199 **2.1 Goal and scope**

200 The goal of this study was to evaluate the environmental performances of the ~~developed~~ CCUS supply chains  
201 ~~(at national large scale)~~ producing ~~different various~~ products in Germany and methane in Italy (Leonzio et al.,  
202 2019; Leonzio and Zondervan, 2020). It was necessary to demonstrate that the suggested CCUS supply chains  
203 achieve the target set by ~~the~~ European environmental policies ~~–especially in terms of~~ carbon dioxide  
204 emissions as defined in Gracevea et al.(2017) for Italy and in Ochoa Bique et al.(2018) for Germany. A  
205 sensitivity analysis was carried out to verify the influence of utilization and storage sections on the  
206 environmental impact and, for a more complete analysis, different impact categories were considered:  
207 ~~(acidification potential (AP), eutrophication potential (EP), ozone depletion potential (ODP), abiotic depletion~~  
208 ~~potential (ADP) fossil and elements, fresh water aquatic ecotoxicity potential (FAETP), human toxicity~~  
209 ~~potential (HTP), marine aquatic ecotoxicity potential (MAETP), photochemical ozone creation potential~~  
210 ~~(POCP), terrestrial ecotoxicity potential (TETP)). In this case, then, e~~Conditions ensuring higher sustainability  
211 ~~have been were~~ identified.

212 **2.1.1 Functional unit**

213 The ~~considered~~ CCUS supply chains ~~considered here~~ have ~~multiple -functionalities in recycling carbon~~  
214 ~~dioxide into a valuable products~~ (von der Assen et al., 2014a). In order to define the functional unit, a system  
215 expansion methodology was applied. ~~This~~ allows ~~ing~~ the joint evaluation of all ~~functions~~ ~~(where a function in~~  
216 ~~LCA is expressing the recycling of carbon dioxide in different valuable products and/or the co-production of~~  
217 ~~multiple valuable products); -since~~ the functional unit was expanded to contain all functions ~~(e.g. a sum of the~~  
218 ~~single functions is considered according to the principle of the LCA for multi-functional problems) (in this~~  
219 ~~case all valuable products)~~ (Fernandez-Dacosta et al., 2018).

220 ~~Then the functional unit is defined as an harmonized basket provided by the a combination of all products to~~  
221 ~~be produced. With these considerations, For for~~ the CCUS supply chain in Germany (Leonzio et al.,2019) the  
222 functional unit is the following, as defined in Table 4: 76.7 Mtonne of cement+1.22·10<sup>11</sup> kWh of  
223 electricity+13.6 Mtonne of iron and steel+4.79 Mtonne of concrete curing+19.4 Mtonne of wheat+0.378  
224 Mtonne of treated lignin+11 Mtonne of polyurethane+120 Mtonne of calcium carbonate+1.34 Mtonne of  
225 urea+0.846 Mtonne of methanol+19.2 Mtonne of concrete by red mud+20.3 Mtonne of stored CO<sub>2</sub>.

226 Table 4 Definition of the functional unit for the CCUS supply chain of Germany

|                            |                       |
|----------------------------|-----------------------|
| Cement (Mtonne)            | 76.7                  |
| Electricity (kWh)          | 1.22×10 <sup>11</sup> |
| Iron and steel (Mtonne)    | 13.6                  |
| Concrete curing (Mtonne)   | 4.79                  |
| Wheat (Mtonne)             | 19.4                  |
| Lignin (Mtonne)            | 0.378                 |
| Polyurethane (Mtonne)      | 11                    |
| Calcium carbonate (Mtonne) | 120                   |

**Commentato [BD11]:** Do you mean 'multiple functional units'?

**Commentato [GL12R11]:** No, multi-functionalities is a technical term.

**Commentato [BD13]:** What does 'function' mean here? It needs to be defined. It seems to be more than just a 'functon' but more like a set of operations considered as a system?

**Commentato [GL14R13]:** I defined what function means in the LCA

**Commentato [BD15]:** This also doesn't make sense. Why is a 'functional unit' a set of targets? Maybe this is common usage for LCA but it needs to be explained for the readers who may not be familiar with it.

**Commentato [GL16R15]:** Thanks. Explained in the above paragraph.



|                                 |       |
|---------------------------------|-------|
| Urea (Mtonne)                   | 1.34  |
| Methanol (Mtonne)               | 0.846 |
| Concrete by red mud (Mtonne)    | 19.2  |
| Stored CO <sub>2</sub> (Mtonne) | 20.3  |

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228 For the CCUS supply chain in Italy (Leonzio and Zondervan, 2020) the functional unit is, ~~instead,~~ the  
 229 following, as in Table 5: 66.92 Mtonne of steel+2.25·10<sup>10</sup> kWh of electricity+16.1 Mtonne of methane+32.8  
 230 Mtonne of stored CO<sub>2</sub>. In ~~both cases of both countries,~~ the amount of products and that of stored carbon dioxide  
 231 were ~~considered, keeping in mind the results were those determined provided~~ by the optimization of these  
 232 systems (Leonzio et al., 2019, and Leonzio and Zondervan, 2020) ~~in AIMMS (Advanced Interactive~~  
 233 ~~Multidimensional Modeling System).~~

234 Table 5 Definition of the functional unit for the CCUS supply chain of Italy

|                                 |                       |
|---------------------------------|-----------------------|
| Iron and steel (Mtonne)         | 66.92                 |
| Electricity (kWh)               | 2.25×10 <sup>10</sup> |
| Methane (Mtonne)                | 16.1                  |
| Stored CO <sub>2</sub> (Mtonne) | 32.8                  |

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236 As Table 4 and 5 show, a definition of functional unit in absolute terms was considered ~~for this work. (referred~~  
 237 ~~to the whole amount of each product, as obtained by the optimization of the respective supply chain in~~  
 238 ~~AIMMS), according to the goal of this research, that is the LCA of the supply chains optimized in AIMMS,~~  
 239 ~~addressed to verify the effective reduction of carbon dioxide emissions compared to the environmental target.~~  
 240 |

241 **2.1.2 System boundaries**

242 Cradle-to-gate analyses were performed for the supply chains ~~(the use and disposal phases of carbon-dioxide-~~  
 243 ~~based products were not considered in the LCA), where e~~ Carbon dioxide was ~~also~~ considered as a feedstock  
 244 (economic flow) and not only as an emission (von der Assen et al., 2014a) ~~(the use and disposal of carbon-~~  
 245 ~~dioxide based products was not considered in these analyses).~~ System boundaries, describing which processes  
 246 of the supply chain are included in the assessment, for the CCUS framework in Germany are shown in Figure  
 247 2. The CCUS supply chain of Germany ~~taken into consideration~~ in this environmental analysis is that described  
 248 in the work of Leonzio et al. (2019), ~~where T~~ the location of carbon dioxide source and utilization sites was  
 249 fixed.

250 According to the economic optimization ~~performed before,~~ the selected carbon dioxide sources ~~on for~~ the  
 251 whole national territory ~~w~~are: Dresden, Wiesbaden, Berlin, Munich, Potsdam, Magdeburg, Saarbrücken.  
 252 These are representative of different kind of industries producing ~~the~~ flue gas.

253 ~~Then for the LCA, at the u~~Upstream of the system boundaries, three different ~~inlets~~ inputs are present: power  
 254 plants (Wiesbaden, Berlin, Potsdam), cements plants (Dresden, Saarbrücken) and steel and iron plants

**Commentato [BD17]:** This is very confusing and doesn't add anything.

**Commentato [BD18R17]:**

**Commentato [GL19R17]:** Ok.

**Commentato [BD20]:** Which analyses? Later in the paper products are considered.

**Commentato [GL21R20]:** I'm referring to the LCA analysis, I changed it. I mean the use and disposal phases of products obtained from CO2 (I'm not considering the use of methanol for example but just only its production phase).

**Commentato [BD22]:** I think this would be better as 'inputs' unless it is a specific term commonly used

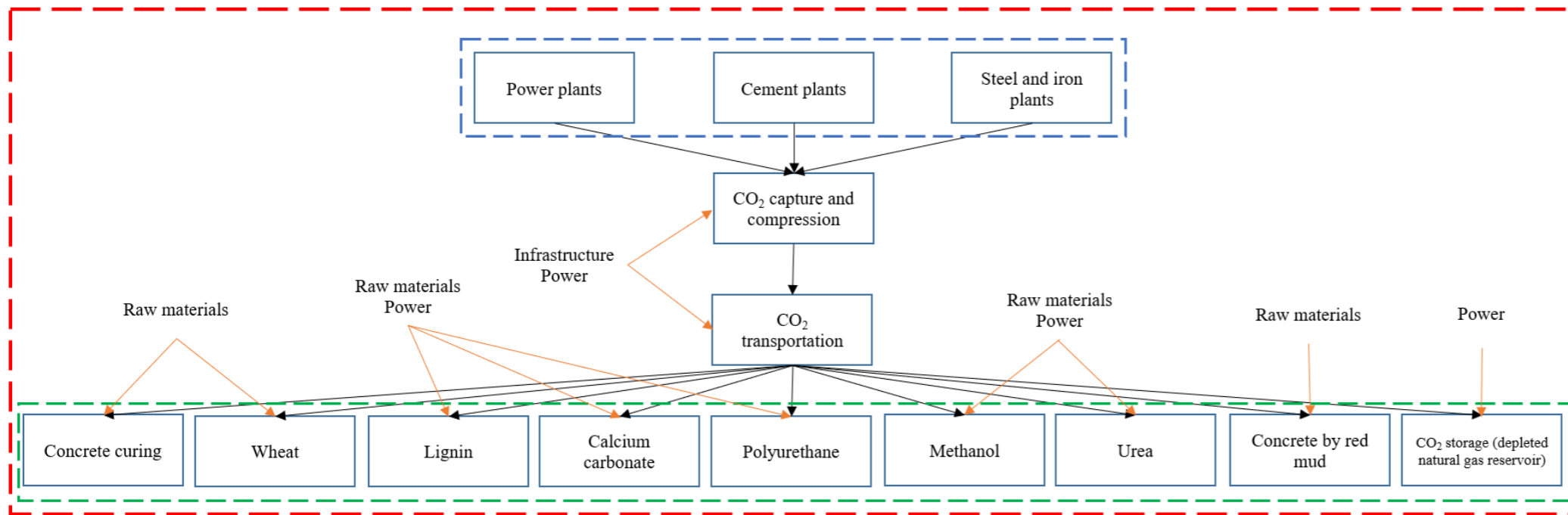
**Commentato [GL23R22]:** Ok

255 (Munich, Magdeburg). Downstream of the storage and utilization processes, where the captured carbon dioxide  
256 is used or stored, nine ~~outlet-output~~ streams are present, namely different products of carbon dioxide utilization  
257 routes (methanol, urea, concrete curing, concrete by red mud, wheat, polyurethane, calcium carbonate, lignin)  
258 and the stored carbon dioxide.

259 The storage site is located in Altmark, the concrete curing sites in Ennigerloh and Hannover, the wheat  
260 cultivation sites in Munich and Hannover, the lignin utilization sites in Cologne and Münchsmünster, the  
261 polyurethane production sites in Schwarzheide and Leverkusen, the calcium carbonate production sites in  
262 Salzgitter and Bremen, the urea production sites in Kassel and Hagen, the methanol production sites in Leuna  
263 and Wesseling, and the concrete production sites by red mud in Rackwitz and Hamburg (the amount of each  
264 carbon dioxide based product and the amount of stored carbon dioxide is that provided in the functional unit).

265 The utilization routes were chosen according to the potential ~~foref~~ different utilization options of carbon  
266 dioxide in Germany, as suggested in the literature (Patricio et al., 2017). Carbon dioxide capture and  
267 compression and carbon dioxide transportation were considered to be inside within the up- and downstream  
268 processes.

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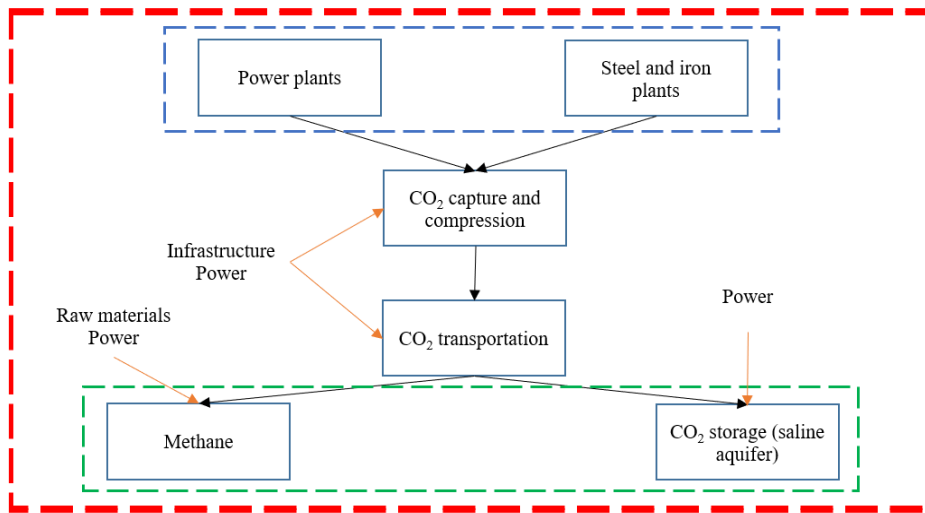
286 Figure 2 System boundaries for the CCUS supply chain in Germany - red line: system boundaries; green line: downstream processes (production of CO<sub>2</sub>-based compounds and CO<sub>2</sub> storage); blue line: upstream processes

287 Figure 3 shows the system boundaries for the CCUS supply chain in Italy. The CCUS supply chain of Italy is  
 288 that described in the work of Leonzio and Zondervan (2020), where carbon dioxide sources and the utilization  
 289 site are fixed as a result of the economic optimization. Throughout the whole national territory, the selected  
 290 carbon dioxide sources for the optimal supply chain are the following: Puglia, Lombardy, Emilia Romagna  
 291 and Piedmont, with different types of industry producing ~~the~~ flue gas.

292 Inside the system boundaries, flue gas sources are present ~~at the~~ upstream: ~~such as~~ a power plant (Emilia  
 293 Romagna) and iron and steel plants (Puglia, Lombardy, Piedmont). Downstream of the utilization process and  
 294 storage section, methane and stored carbon dioxide are considered. The utilization site is located in Verbania,  
 295 while the storage site ~~is in the~~ off-shore ~~in the~~ Adriatic sea saline aquifer. ~~(the amount of methane and the amount~~  
 296 ~~of stored carbon dioxide is that provided in the functional unit).~~

297 The ~~noticeable~~ potential for the application of power to gas plants in Italy was reported by Colbertaldo et al.  
 298 (2018) and Guandalini et al. (2017). Moreover, the production of methane is specifically selected for the Italian  
 299 regions, ~~because~~ the potential of methanol production, ~~investigated already in the literature,~~ is very low there  
 300 (Patricio et al., 2017). On the other hand, Italy would have the opportunity to satisfy ~~the its~~ national methane  
 301 demand by hydrogenation of CO<sub>2</sub>. In addition, an existing ~~capillary~~ network for CH<sub>4</sub> distribution is present in  
 302 Italy and a power-to-gas system is achievable on ~~a~~ large scale with a high technical readiness level. Also in  
 303 this case, carbon dioxide capture, compression and transportation are included between the upstream and  
 304 downstream processes.

Commentato [BD24]: Not necessary to say this here.  
 Commentato [GL25R24]: Ok!



305  
 306 Figure 3 System boundaries for the CCUS supply chain in Italy - red line: system boundaries; green line:  
 307 downstream processes (production of methane and CO<sub>2</sub> storage); blue line: upstream processes

308

309 ~~Then, for~~ both supply chains, the utilization options ~~were~~ chosen ~~whereas~~ the most economically appealing  
310 carbon-dioxide-based products for the respective Countries, ~~according to the literature~~. Only methane is taken  
311 into account in the frameworks ~~for~~ Italy, while methanol, urea, concrete curing, concrete by red mud, wheat,  
312 polyurethane, calcium carbonate, lignin are proposed ~~for~~ the German supply chain ~~of Germany~~.  
313 In both supply chains, system boundaries included ~~also~~ the construction of plants related to carbon dioxide  
314 sources, the extraction or production of raw materials and their transportation calculated using the database ~~of~~  
315 in the GaBi software (Thinkstep, 2019). The production and transport of raw materials for the infrastructure  
316 needed for carbon dioxide pipelines were also considered, ~~according to literature sources~~ (Koornneef et al.,  
317 2008). Infrastructure needs were considered only for carbon dioxide capture with MEA absorption, due to the  
318 scarce availability of data for different capture technologies (Giordano et al., 2018). For the utilization  
319 processes, infrastructure data ~~was~~ not available, ~~h~~ However, the production of raw materials was considered  
320 inside the system boundary. Natural infrastructures to store CO<sub>2</sub> are available in both cases examined here (a  
321 saline aquifer and a depleted natural gas reservoir). Only power needed for the storage process is taken into  
322 account (Wildbolz, 2007).

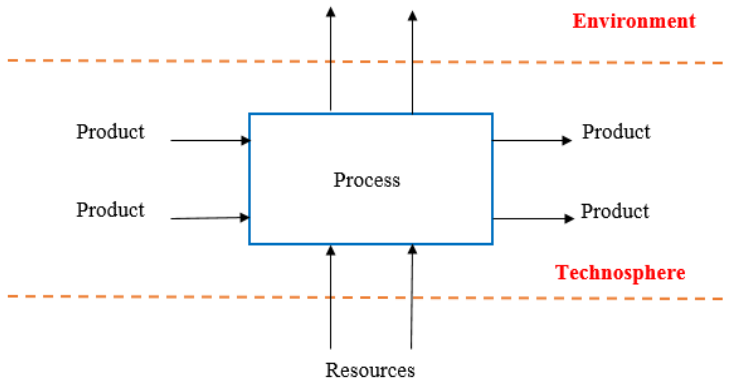
## 323 2.2 Life cycle inventory phase

324 In the LCI phase, input and output data for all processes of the CCUS supply chains were provided. ~~In~~  
325 ~~particular,~~ The results for the large-scale supply chains obtained by the optimization ~~and design with AIMMS~~  
326 ~~software~~ were ~~used~~ ~~considered~~ (Leonzio et al., 2019; Leonzio and Zondervan, 2020). Based on ~~this~~ ~~ese~~ process  
327 data, an inventory list for the complete life cycle was calculated. ~~In particular,~~ ~~a~~ All elementary flows entering  
328 the process (technosphere) from nature (environment) in the form of resources, and those leaving the process  
329 in the form of resources, deposited goods, emissions to air, fresh water, sea water, agricultural and industrial  
330 soil were taken into account, as shown in Figure 4.

331

332

Resources, deposited goods, emissions to air, emissions to fresh water,  
emissions to sea water, emissions to agricultural and industrial soil



333

334 Figure 4 Elementary flows entering and leaving the process

335

336 ~~An inventory analysis of processes that are missing in the database of GaBi software (Thinkstep, 2019) was~~  
 337 ~~considered here, by integration data already reported in the literature. In fact, each literature work takes into~~  
 338 ~~account different aspects of the process, then their integration allows to have a more complete vision of~~  
 339 ~~inventory data. Even if different researches are based on different assumptions, a real process is described~~  
 340 ~~underlining different aspects that are integrated in our inventory analysis;~~

341 ~~These processes were especially important for carbon dioxide utilization, storage and transportation.~~ For the  
 342 CCUS supply chain of Germany (Leonzio et al., 2019), an inventory analysis was performed for production  
 343 from carbon dioxide of methanol, calcium carbonate, polyurethane, urea, wheat, concrete curing, concrete by  
 344 red mud and lignin treatment with carbon dioxide. Tables 6 and 7 show respectively the inventory analysis for  
 345 methanol production by carbon dioxide hydrogenation and for hydrogen production by water electrolysis,  
 346 ~~considering using~~ the work of Biernacki et al. (2018), Michailos et al. (2018), Kajaste et al. (2018), and Matzen  
 347 and Demirel (2016). ~~For different inputs appearing in those Tables. It was also considered T~~the recycle of  
 348 unconverted gases to the methanol reactor, after separation of water and methanol ~~was also considered,~~ with  
 349 an efficiency of 80%. In summary, 1.7 ~~tonne~~ of carbon dioxide are consumed per ton of produced methanol  
 350 (Patricio et al., 2017). ~~Regarding the C-catalyst (aluminum, copper and zinc oxide), it is required (as an input);~~  
 351 ~~however but~~ it is not consumed.

352

353

**Commentato [BD26]:** I have read this paragraph twice and I still have no idea what you are trying to say. I suggest you just delete it.

**Commentato [GL27R26]:** I mean that the main database for the inventory is gabi. However not all processes are defined there, then literature works were considered for processes missing in gabi. But we can delete this section.

**Commentato [BD28]:** Shouldn't this be tonne? (always). It is a different measure than ton (which is Imperial units)

**Commentato [GL29R28]:** Ok, I changed it

354

355 Table 6 Inventory analysis for ~~the~~ methanol synthesis via carbon dioxide hydrogenation in the CCUS supply  
 356 chain of Germany (Biernacki et al., 2018; Michailos et al., 2018; Kajaste et al., 2018; Matzen and Demirel,  
 357 2016; Patricio et al., 2017)

| Input of the process  |                         |
|-----------------------|-------------------------|
| H <sub>2</sub>        | 0.23 <del>t</del> tonne |
| CO <sub>2</sub>       | 1.70 <del>t</del> tonne |
| Aluminum oxide        | 0.01 <del>t</del> tonne |
| Copper oxide          | 0.08 <del>t</del> tonne |
| Zinc oxide            | 0.04 <del>t</del> tonne |
| Water                 | 5.45 <del>t</del> tonne |
| Energy                | 0.13 MWh                |
| Output of the process |                         |
| Wastewater            | 0.68 m <sup>3</sup>     |
| CO <sub>2</sub>       | 0.34 <del>t</del> tonne |
| Methanol              | 1 <del>t</del> tonne    |

358

359 Table 7 Inventory analysis for the electrolyzer in the methanol production process in the CCUS supply chain  
 360 of Germany (Biernacki et al., 2018; Michailos et al., 2018; Kajaste et al., 2018; Matzen and Demirel, 2016;  
 361 Patricio et al., 2017)

| Input of the process          |                         |
|-------------------------------|-------------------------|
| Water                         | 2.22 <del>t</del> tonne |
| Traditional energy            | 141.96 kWh              |
| Renewable energy              | 6.11 kWh                |
| Output of the process         |                         |
| Oxygen                        | 1.97 <del>t</del> tonne |
| H <sub>2</sub>                | 0.23 <del>t</del> tonne |
| Waste water                   | 0.12 m <sup>3</sup>     |
| VOC                           | 5.23 g                  |
| CO                            | 47.67 g                 |
| NO <sub>x</sub>               | 41.31 g                 |
| PM <sub>10</sub>              | 15.16 g                 |
| PM <sub>2.5</sub>             | 7.50 g                  |
| SO <sub>x</sub>               | 276.67 g                |
| CH <sub>4</sub>               | 47.06 g                 |
| CO <sub>2</sub>               | 28.22 kg                |
| SF <sub>6</sub>               | 0.92 mg                 |
| C <sub>2</sub> F <sub>6</sub> | 0.10 g                  |
| Black carbon                  | 0.25 g                  |
| POC                           | 0.48 g                  |

362

363 Table 8 shows the inventory analysis for calcium carbonate production from carbon dioxide, ~~taking into~~  
 364 ~~account the literature works of~~ based on Mattila et al. (2014) and Zappa (2014) and considering that the ratio  
 365 between ~~the each~~ tonne of used carbon dioxide and ~~the~~ tonne of steel slag is 0.42. An inventory analysis for

15

366 lignin treatment with carbon dioxide is presented in Table 9 ~~based on, according to the work of~~ Bernier and  
 367 Lavigne (2013) and considering that 0.22 tonne of carbon dioxide per ton of lignin are utilized (Patricio et al.,  
 368 2017).

369 Table 8 Inventory analysis for the calcium carbonate production process from carbon dioxide in the CCUS  
 370 supply chain of Germany (Mattila et al., 2014; Zappa, 2014)

| Input of the process       |             |
|----------------------------|-------------|
| Steel slag                 | 2.60 ttonne |
| CO <sub>2</sub>            | 1.1 ttonne  |
| NH <sub>4</sub> Cl solvent | 0.03 ttonne |
| Electricity                | 107.40 kWh  |
| Water                      | 2.10 ttonne |
| Steam                      | 37500 MJ    |
| Output of the process      |             |
| Calcium carbonate          | 1.00 ttonne |
| Waste water, steel slag    | 2.01 ttonne |

371

372 Table 9 Inventory analysis for the lignin treatment process with carbon dioxide in the CCUS supply chain of  
 373 Germany (Bernier and Lavigne; 2013; Patricio et al., 2017)

| Input of the process           |                              |
|--------------------------------|------------------------------|
| Natural gas                    | 0.46 ttonne                  |
| CO <sub>2</sub>                | 0.22 ttonne                  |
| H <sub>2</sub> SO <sub>4</sub> | 0.17 ttonne                  |
| NaOH                           | 0.08 ttonne                  |
| CaCO <sub>3</sub>              | 0.17 ttonne                  |
| Water                          | 3.56 ttonne                  |
| Electricity                    | 7.33 kWh                     |
| Output of the process          |                              |
| SO <sub>2</sub>                | 6.75×10 <sup>-9</sup> ttonne |
| NO <sub>x</sub>                | 3.38×10 <sup>-7</sup> ttonne |
| CO                             | 3.82×10 <sup>-7</sup> ttonne |
| Lignin                         | 1 tonne                      |

374

375 Polyurethane is produced ~~by-from~~ polyols and isocyanate. The ~~former-first~~ reactant is obtained by carbon  
 376 dioxide, while the latter one is obtained ~~by-from~~ carbon monoxide produced by methane steam reforming. All  
 377 inputs and outputs for these processes are shown in Table 10 ~~based on, according to the work of~~ von der Assen  
 378 et al. (2015). For polyurethane production from carbon dioxide, the ratio between used carbon dioxide and  
 379 polyurethane is 0.3 tonne/tonne (Patricio et al., 2017). More information about the polyurethane production  
 380 route that is taken into account here is ~~made~~-available in the Supplementary Material.

381



382 Table 10 Inventory analysis for the polyurethane production from carbon dioxide in the CCUS supply chain  
 383 of Germany (Von der Assen et al., 2015; Patricio et al., 2017)

| Polyurethane production (flexible foam) |                            |
|---|----------------------------|
| <b>Input of the process</b>             |                            |
| Polyols                                 | 0.713 kg                   |
| Electricity                             | 1.5 MJ                     |
| TDI                                     | 0.285 kg                   |
| <b>Output of the process</b>            |                            |
| Flexible foam                           | 1 kg                       |
| GW                                      | 0.051 kgCO <sub>2-eq</sub> |
| Isocyanate production                   |                            |
| <b>Input of the process</b>             |                            |
| Toluene                                 | 0.15 kg                    |
| Electricity                             | 3.77 MJ                    |
| CO                                      | 0.09 kg                    |
| Nitric acid                             | 0.21 kg                    |
| <b>Output of the process</b>            |                            |
| TDI                                     | 0.285 kg                   |
| Steam reforming                         |                            |
| <b>Input of the process</b>             |                            |
| CH <sub>4</sub>                         | 0.066 kg                   |
| Electricity                             | 0.353 MJ                   |
| Heat                                    | 0.747 MJ                   |
| <b>Output of the process</b>            |                            |
| H <sub>2</sub>                          | 0.020 kg                   |
| CO                                      | 0.092 kg                   |
| Polyols production                      |                            |
| <b>Input of the process</b>             |                            |
| Starter                                 | 0.019 kg                   |
| Propylen oxide                          | 0.395 kg                   |
| CO <sub>2</sub>                         | 0.299 kg                   |
| <b>Output of the process</b>            |                            |
| Polyols                                 | 0.713 kg                   |

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390 Table 11 Inventory analysis for urea production from carbon dioxide in the CCUS supply chain of Germany  
 391 (Antonetti et al., 2017; Patricio et al., 2017)

| <b>Input of the process</b> |  |
|-----------------------------|--|
|-----------------------------|--|

|                              |                 |             |
|------------------------------|-----------------|-------------|
| NH <sub>3</sub>              | 0.57            | tonne       |
| CO <sub>2</sub>              | 0.74            | tonne       |
| Energy                       | 0.05            | MWh         |
| <b>Output of the process</b> |                 |             |
| NH <sub>3</sub> emissions    | 0.004           | tonne       |
| Wastewater                   | 0.48            | tonne       |
|                              | NH <sub>3</sub> | 0.03 tonne  |
|                              | CO <sub>2</sub> | 0.02 tonne  |
|                              | Urea            | 0.005 tonne |
|                              | water           | 0.43 tonne  |
| Urea                         | 1               | tonne       |

392

393 An inventory analysis for urea production from carbon dioxide is shown in Table 11 ~~based on, according to~~  
 394 ~~the work of~~ Antonetti et al. (2017). Here 0.74 tonne of carbon dioxide are used to produce 1 tonne of urea  
 395 (Patricio et al., 2017).

396 ~~CO<sub>2</sub> can also be utilized at large scale in agricultural processes. The environmental burden and inventory~~  
 397 ~~analysis for wheat growing enhanced by carbon dioxide is shown in Table 12 based on, considering the works~~  
 398 ~~of Biswas et al. (2010, 2008). According to tests of free air concentration enrichment (FACE) of carbon dioxide~~  
 399 ~~performed around the world, this utilization route is not so as effective as preliminary laboratory experiments~~  
 400 ~~were announcing showed. CO<sub>2</sub> concentration cannot be increased much above its value in the atmosphere (Erda~~  
 401 ~~et al. 2005), because the absorption rate of carbon by photosynthesis increases at the expenses of Nitrogen~~  
 402 ~~(proteins) and additional nutrients, changing the quality of biomass grown. For this reason, the contribution of~~  
 403 ~~CO<sub>2</sub>, in addition to that already available in the atmosphere, can be only marginal and was evaluated as 500~~  
 404 ~~mg per kg of wheat produced (Leonzio et al., 2019).~~

405

406 ~~Table 12 Inventory analysis for wheat production in the CCUS supply chain of Germany (Biswas et al.,~~  
 407 ~~2010; 2008; Leonzio et al., 2019)~~

|                              |     |                      |
|------------------------------|-----|----------------------|
| <b>Input of the process</b>  |     |                      |
| CO <sub>2</sub>              | 0.5 | kg                   |
| <b>Output of the process</b> |     |                      |
| Wheat                        | 1   | ton                  |
| GW                           | 275 | kgCO <sub>2-eq</sub> |

408

409 Inventory analyses for concrete produced by red mud and concrete curing are shown respectively in Tables 13  
 410 12 and 1413, ~~comparing using~~ data reported by Nikbin et al. (2018) and Gursel and Horvath (2012). The GWP  
 411 and cumulative energy demand (CED) are respectively ~~of~~ 330.74 kgCO<sub>2-eq</sub> and 2848.5 MJ for concrete  
 412 production by red mud (1 tonne) (Nikbin et al., 2018). The GWP and CED are, ~~instead,~~ respectively of 292  
 413 kgCO<sub>2-eq</sub> and 1374.68 MJ for concrete curing (1 tonne) (Nikbin et al., 2018; www.carboncure.com). In concrete  
 414 curing, 0.03 tonne of carbon dioxide are required for 1 tonne of concrete (Patricio et al., 2017), while in

**ha formattato:** Tipo di carattere: (Predefinito) Times New Roman, Inglese (Stati Uniti)

**Commentato [BD30]:** Up to now everything has been about industrial utilisation. You seem to have switched to agriculture. You need to introduce this for example 'CO2 can also be utilised at large scale in agricultural processes.' It would be better if this paragraph came right at the end of the section since there are more industrial aspects considered after this.

**Commentato [GL31R30]:** I see that you have already added the sentence.

**ha formattato:** Inglese (Stati Uniti)

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415 concrete by red mud production the ratio between ~~the one~~ tonne of carbon dioxide and ~~one~~the tonne of red  
 416 mud is 0.17.

417

418 Table ~~13-12~~ Inventory analysis for concrete production by red mud and carbon dioxide in the CCUS supply  
 419 chain of Germany (Nikbin et al., 2018; Gursel and Horvath, 2012; Patricio et al., 2017)

| Input of the process  |                                 |
|-----------------------|---------------------------------|
| Cement                | 0.222 <del>tonne</del> tonne    |
| Red mud               | 0.074 <del>tonne</del> tonne    |
| Coarse Agg            | 0.129 <del>tonne</del> tonne    |
| Fine Agg.             | 0.106 <del>tonne</del> tonne    |
| Leca                  | 0.197 <del>tonne</del> tonne    |
| Limestone             | 0.118 <del>tonne</del> tonne    |
| Water                 | 0.150 <del>tonne</del> tonne    |
| Superplasticizer      | 0.004 <del>tonne</del> tonne    |
| CO <sub>2</sub>       | 0.013 <del>tonne</del> tonne    |
| Output of the process |                                 |
| Concrete              | 1 <del>tonne</del> tonne        |
| CO                    | 0.04619 <del>tonne</del> tonne  |
| Lead                  | 0.000012 <del>tonne</del> tonne |
| NO <sub>x</sub>       | 0.00075 <del>tonne</del> tonne  |
| PM <sub>10</sub>      | 0.00002 <del>tonne</del> tonne  |
| SO <sub>2</sub>       | 0.00076 <del>tonne</del> tonne  |
| VOC                   | 0.00057 <del>tonne</del> tonne  |

420

421 Table ~~14-13~~ Inventory analysis for concrete curing in the CCUS supply chain of Germany (Nikbin et al., 2018;  
 422 Gursel and Horvath, 2012; Patricio et al., 2017)

| Input of the process  |                                |
|-----------------------|--------------------------------|
| Cement                | 0.285 <del>tonne</del> tonne   |
| Water                 | 0.145 <del>tonne</del> tonne   |
| Fine aggregates       | 0.118 <del>tonne</del> tonne   |
| Coarse aggregates     | 0.145 <del>tonne</del> tonne   |
| Leca                  | 0.190 <del>tonne</del> tonne   |
| Limestone             | 0.114 <del>tonne</del> tonne   |
| Superplasticize       | 0.003 <del>tonne</del> tonne   |
| CO <sub>2</sub>       | 0.030 <del>tonne</del> tonne   |
| Output of the process |                                |
| CO                    | 0.056 <del>tonne</del> tonne   |
| Lead                  | 0.00001 <del>tonne</del> tonne |
| Nox                   | 0.001 <del>tonne</del> tonne   |
| PM <sub>10</sub>      | 0.00003 <del>tonne</del> tonne |
| SO <sub>2</sub>       | 0.001 <del>tonne</del> tonne   |
| VOC                   | 0.001 <del>tonne</del> tonne   |
| Concrete              | 1.000 <del>tonne</del> tonne   |

423

424 CO<sub>2</sub> can also be utilized at large scale in agricultural processes. The environmental burden and inventory  
 425 analysis for wheat growing enhanced by carbon dioxide is shown in Table 14 based on Biswas et al. (2010,  
 426 2008). According to tests of free air concentration enrichment (FACE) of carbon dioxide performed around  
 427 the world, this utilization route is not as effective as preliminary laboratory experiments showed. CO<sub>2</sub>  
 428 concentration cannot be increased much above its value in the atmosphere (Erda et al. 2005), because the  
 429 absorption rate of carbon by photosynthesis increases at the expenses of Nitrogen (proteins) and additional  
 430 nutrients, changing the quality of biomass grown. For this reason, the contribution of CO<sub>2</sub>, in addition to that  
 431 already available in the atmosphere, can be only marginal and was evaluated as 500 mg per kg of wheat  
 432 produced (Leonzio et al., 2019).

433  
 434 Table 14 Inventory analysis for wheat production in the CCUS supply chain of Germany (Biswas et al.,  
 435 2010; 2008; Leonzio et al., 2019)

| <u>Input of the process</u>  |            |                            |
|------------------------------|------------|----------------------------|
| <u>CO<sub>2</sub></u>        | <u>0.5</u> | <u>kg</u>                  |
| <u>Output of the process</u> |            |                            |
| <u>Wheat</u>                 | <u>1</u>   | <u>tonne</u>               |
| <u>GW</u>                    | <u>275</u> | <u>kgCO<sub>2</sub>-eq</u> |

436  
 437  
 438 In the Italian CCUS supply chain ~~of Italy~~ (Leonzio and Zondervan, 2020); methane is produced from carbon  
 439 dioxide with a power to gas process (by means of hydrogen produced by water electrolysis exploiting  
 440 renewable energy sources). Table 15 shows the inventory analysis for the methanation process; (using the  
 441 Sabatier reaction) assuming complete CO<sub>2</sub> conversion to methane (Reiter et al., 2015; Sternberg and Bardow,  
 442 2016).

443 Table 15 Inventory analysis for the methanation process (Sabatier reaction) in the CCUS supply chain of Italy  
 444 (Reiter et al., 2015; Sternberg and Bardow, 2016)

| <u>Input of the process</u>  |                 |
|------------------------------|-----------------|
| <u>CO<sub>2</sub></u>        | <u>2.75 kg</u>  |
| <u>H<sub>2</sub></u>         | <u>0.5 kg</u>   |
| <u>Electricity</u>           | <u>0.33 kWh</u> |
| <u>Output of the process</u> |                 |
| <u>CH<sub>4</sub></u>        | <u>1 kg</u>     |
| <u>Waste heat</u>            | <u>8.26 MJ</u>  |
| <u>H<sub>2</sub>O</u>        | <u>2.29 kg</u>  |

445  
 446  
 447 In both CCUS supply chains considered ~~before-previously~~ (Leonzio et al., 2019; Leonzio and Zondervan,  
 448 2020); carbon dioxide was also stored: it was ~~supposed~~assumed that electrical energy is used to inject carbon

**Commentato [BD32]:** Up to now everything has been about industrial utilisation. You seem to have switched to agriculture. You need to introduce this for example 'CO<sub>2</sub> can also be utilised at large scale in agricultural processes.' It would be better if this paragraph came right at the end of the section since there are more industrial aspects considered after this.

**Commentato [GL33R32]:** I see that you have already added the sentence. I moved this part at the end of the section.

449 dioxide and the required energy is  $-2.86 \cdot 10^{-2}$  kWh/kgCO<sub>2</sub> (Wildbolz, 2007). Regarding carbon dioxide  
450 transportation, infrastructures and energy, data were ~~considered used from according to the work of~~ Koornneef  
451 et al. (2008) and Wildbolz (2007), respectively. It was ~~supposed-assumed~~ that carbon dioxide recompression  
452 is necessary for a distance exceeding 400 km and ~~that~~ the associated energy consumption is 0.011 kWh/(tonne  
453 km) (Wildbolz, 2007). No leakage emissions were considered due to their negligible value (Bouman et al.,  
454 2015).

455 For the inventory analysis of carbon dioxide capture with ~~piperazine~~ absorption, the energy requirement was  
456 ~~considered estimated~~: von der Assen et al. (2015) suggested a value of 0.80 GJ/tonneCO<sub>2</sub>, while 0.86  
457 GJ/tonneCO<sub>2</sub> are necessary for the absorption of carbon dioxide with MEA. Infrastructures and emissions data  
458 for this last technology were proposed by Giordano et al. (2018).

459 The LCI results, provided by GaBi software, ~~about for the German CCUS supply chain in Germany~~ (Leonzio  
460 et al., 2019) are classified as input (resources) and output (resources, deposited goods, emissions to air, fresh  
461 water, sea water, agricultural soil and industrial soil). ~~It is worth noticing that, in~~ the output, the greatest  
462 contribution to elementary flows is made ~~of by~~ the emissions to fresh water (63.4%) followed by the emissions  
463 to air (35.8%). Other terms are negligible. These elementary flows can be expressed also in kgCO<sub>2-eq</sub>. In the  
464 input,  $5.24 \times 10^{11}$  kgCO<sub>2-eq</sub> ~~of resources~~ are present. In the output,  $7.08 \times 10^{11}$  kgCO<sub>2-eq</sub> of emissions to air are  
465 ~~produced calculated~~. ~~As a weak point in this analysis, it was found that the s~~ Steam production in the calcium  
466 carbonate process and carbon dioxide source in Munich provides the highest contribution to the emissions to  
467 air.

468  
469 For each carbon dioxide source, carbon dioxide (as a feedstock sent to storage or utilization) is co-produced  
470 with the main product of the industry emitting flue gas. To allocate the environmental impact between the  
471 main product and the co-product, the price allocation method was adopted. The prices for carbon dioxide,  
472 electricity, cement and steel are respectively 80 €/tonne, 0.15 €/kWh, 80 €/tonne and 589 €/tonne (Focus  
473 Economics, 2019; Boyer and Ponsard, 2013; Europe, 2019; OECD, 2013).

474 The LCI results, ~~then the elementary flows discussed for the previous supply chains~~, were also obtained  
475 ~~using by the~~ GaBi software for the ~~Italian CCUS supply chain in Italy~~ (Leonzio and Zondervan, 2020). ~~In the~~  
476 ~~output, t~~ The greatest impact was due to the emissions to fresh water and to air that contributed respectively  
477 ~~for~~ 75.4% and 20.9% to the total output flow. The deposited goods contributed ~~with~~ 2.97% to the total flow,  
478 while other contributions were negligible. Inputs and outputs were expressed also as kgCO<sub>2-eq</sub>: ~~input resources~~  
479 ~~in input w~~ ~~asere~~  $2.83 \times 10^8$  kgCO<sub>2-eq</sub> while emissions to air in the output ~~w~~ ~~asere~~  $9.67 \times 10^{10}$  kgCO<sub>2-eq</sub>. The highest  
480 contribution was due to the carbon dioxide sources in Lombardy and Puglia (iron and steel plants).

481 Also in this case, a price allocation criterion was applied to carbon dioxide sources. The price taken into  
482 account for CO<sub>2</sub>, electricity and steel are respectively ~~of~~ 80 €/tonne, 0.15 €/kWh and 589 €/tonne (Portdata,  
483 2019; Focus Economics, 2019; OECD, 2013).

484

Commentato [BD34]: I don't know what this is. Is it correct?

Commentato [GL35R34]: Yes, it is correct.

485 **3. Results** <https://pre-sustainability.com/articles/consider-your-audience-when-doing-lca/>

486 The results from the of LCA are here discussed in this section for both CCUS supply chains. The magnitude  
487 of the environmental burden was evaluated through two different steps: classification and characterization. In  
488 these steps, the LCI results were combined and organized into the impact categories (classification step) and  
489 then into the impact indicators at the midpoint level of the cause-effect chain that analyzes the environmental  
490 effect due to defined causes (characterization step) using the CML 2001 methodology (Guinee et al., 2002)  
491 implemented in the GaBi software (Thinkstep, 2019) (LCIA phase). In the last phase of this environmental  
492 analysis, the interpretation of previous results in terms of significant issues and sensitivity analysis was  
493 developed (interpretation phase).

494 **3.1 Life cycle impact assessment phase for the German CCUS supply chain of Germany**

495 The environmental impact category that was considered is the Global Warming Potential (GWP), sometimes  
496 also referred to as the GWI or Global Warming Impact (Heijungs, 2014), because the first aim of this  
497 analysis was to determine the ability to meet verify the targets suggested set by the national environmental  
498 policies regarding with respect to carbon dioxide emissions. Results for the other impact categories, like such  
499 as AP, EP, ODP, ADP fossil and elements, FAETP, HTP, MAETP, POCP, and TETP are shown in the  
500 Supplementary Materials (see Table S1).

501 Results showed that the value for GWP was of  $1.94 \times 10^{11}$  kgCO<sub>2-eq</sub>: the CCUS supply chain is able to achieve  
502 what established the target set by in the German environmental policy for 2020 by their Government's  
503 environmental regulations. In fact, the German Federal Ministry for the Environment (2017) stated that in  
504 Germany carbon dioxide emissions should be lower than 751 MtonneCO<sub>2</sub> in by 2020. On the other hand, for  
505 the CCUS of Germany described in Leonzio et al. (2019), in the scheme suggested proposed before total  
506 carbon dioxide emissions were of 640 MtonneCO<sub>2</sub>, which also includes also emissions from sources not  
507 included selected in the optimized chain.

508 The greatest carbon dioxide emissions inside in the CCUS supply chain, come from the carbon dioxide source  
509 in Munich (steel and iron plant) with  $7.85 \times 10^{10}$  kgCO<sub>2-eq</sub>, followed by steam production in the precipitated  
510 calcium carbonate process, with  $1.95 \times 10^{10}$  kgCO<sub>2-eq</sub>, by carbon dioxide source in Potsdam (power plant) with  
511  $1.65 \times 10^{10}$  kgCO<sub>2-eq</sub>, by from the process for the production of propylene oxide in polyurethane production,  
512 with  $1.53 \times 10^{10}$  kgCO<sub>2-eq</sub>, and by the process to produce concrete by red mud, with  $6.42 \times 10^9$  kgCO<sub>2-eq</sub>.

513 **3.2 Life cycle impact assessment phase for the Italian CCUS supply chain of Italy**

514 Also for the Italian CCUS supply chain in Italy (Leonzio and Zondervan, 2020), the goal of the analysis was  
515 again to ensure verify that the supply chain reduces carbon dioxide emissions to a value lower than that  
516 established by the national environmental policy, in this case equal to 275 MtonneCO<sub>2</sub> (Gracceva et al., 2017).  
517 For this reason, only the GWP impact category is considered. Results showed that for this analyzed CCUS  
518 supply chain, the value of GWP was  $9.62 \times 10^{10}$  kgCO<sub>2-eq</sub>. When considering also the additional carbon dioxide

**Commentato [BD36]:** What does this mean? Doesn't seem to be used later?

**Commentato [GL37R36]:** Explained in the following sentence.

**Commentato [BD38]:** midpoint of what?

**Commentato [GL39R38]:** It is a technical term:

Midpoints are considered to be links in the cause-effect chain (environmental mechanism) of an impact category, prior to the endpoints, at which characterization factors or indicators can be derived to reflect the relative importance of emissions or extractions.

**Commentato [BD40]:** It is worth giving the full name at key moments like this

**Commentato [GL41R40]:** Ok!

**Formattato:** SpazioDopo: 8 pt

**Commentato [BD42]:** By whom? Is it your scheme or a German scheme?

**Commentato [GL43R42]:** I explained better.

519 sources not ~~selected-included in~~for the optimized supply chain; the total carbon dioxide emissions were ~~of~~ 249  
520 MtonneCO<sub>2</sub>. A value lower than the target was then-obtained; showing that the proposed ~~approach~~solution is  
521 able to ~~reduce~~ effectively reduce carbon dioxide emissions in Italy. Inside the supply chain, the processes with  
522 a greatest contribution to carbon dioxide emissions are the iron and steel plant in Puglia ( $6.32 \times 10^{10}$  kgCO<sub>2</sub>-  
523 eq) and the iron and steel plant in Lombardy ( $1.09 \times 10^{10}$  kgCO<sub>2</sub>-eq). For a complete analysis, other impact  
524 categories ~~like-such as~~ AP, EP, ODP, ADP fossil and elements, FAETP, MAETP, POCP, TEP ~~were~~ reported  
525 in the Supplementary Materials (see Table S2).

## 526 4. Discussion

### 527 4.1 Interpretation phase for the German CCUS supply chain ~~of Germany~~

528 ~~The interpretation phase involves a sensitivity analysis around the base case to explore the extent to which the~~  
529 ~~results are significant and the way that changes may affect them. From the above~~The results in section 3.1  
530 ~~show, it was noticeable~~ that ~~the~~ significant ~~issues~~ (processes that contribute most to the overall result) were:  
531 the precipitated calcium carbonate process, due to ~~the~~ high environmental impact of steam production, carbon  
532 dioxide sources (in particular Munich, Potsdam), propylene oxide formation in the polyurethane production  
533 section and concrete production by red mud.

534 A sensitivity analysis was carried out to evaluate the relative influence of ~~the~~ storage and utilization sections  
535 ~~inside the topology suggested for~~ within the supply chain. ~~In particular, f~~For carbon dioxide captured from  
536 Magdeburg, the amount that is sent to the storage section is ~~tentatively utilized, in this sensitivity analysis and~~  
537 ~~used at~~ different percentages; for the ~~separate~~ production of different species (concrete by red mud or curing,  
538 wheat, lignin upgrading, urea, methanol, polyurethane and calcium carbonate). ~~With~~ For the three different  
539 case studies, ~~only~~ 25%, 50% and 75% of the ~~whole~~ carbon dioxide originally stored in the base case; was  
540 maintained in the storage section ~~in this sensitivity analysis~~, while the remaining carbon dioxide captured was  
541 sent to utilization; in order to increase the production of ~~the single one~~ product.

542 Results ~~giving the negative or positive change~~ are shown ~~qualitatively~~ in Table 16 (the absolute values  
543 corresponding to the arrows of Table ~~13-16~~ are shown in Tables S3-S10 of the Supplementary Materials); ~~f~~For  
544 a complete picture of the environmental impact, all impact categories were considered (Supplementary  
545 Material). ~~In fact, w~~ While the GWP is expected to be ~~reduced~~ increased by increasing the utilization rate of  
546 carbon dioxide, other impacts could be increased, constant or decreased (Cuellar-Franca and Azapagic, 2015).  
547 For a more detailed analysis see the Supplementary Materials (Interpretation phase).

548  
549  
550  
551

ha formattato: Tipo di carattere: Non Grassetto

552

553 Table 16 Sensitivity analysis: trends resulting for different impact categories when increasing the carbon  
 554 dioxide utilization rate in each utilization section of the supply chain for Germany; arrows indicate variation  
 555 in -direction and intensity for each impact category with reference to the base case ( low variation (<5%), constant value, / medium variation (<50%), high variation (>50%))

|                     | GWP | AP | EP | ODP | ADP elements | ADP fossil | FAETP | HTP | MAETP | POCP | TETP |
|---------------------|-----|----|----|-----|--------------|------------|-------|-----|-------|------|------|
| Methanol            |     |    |    |     |              |            |       |     |       |      |      |
| Concrete curing     |     |    |    |     |              |            |       |     |       |      |      |
| Urea                |     |    |    |     |              |            |       |     |       |      |      |
| Wheat               |     |    |    |     |              |            |       |     |       |      |      |
| Lignin treatment    |     |    |    |     |              |            |       |     |       |      |      |
| Polyurethane        |     |    |    |     |              |            |       |     |       |      |      |
| Calcium carbonate   |     |    |    |     |              |            |       |     |       |      |      |
| Concrete by red mud |     |    |    |     |              |            |       |     |       |      |      |

557

558

559 The sensitivity analysis suggested that the storage site is important inside for the German CCUS supply chain  
 560 in order to reduce the environmental impact; in terms of GWP. In fact, in all cases, the GWP was increased  
 561 raised by increasing the amount of carbon dioxide sent to the utilization section, while keeping constant the  
 562 amount of captured carbon dioxide. Only a few impact categories were reduced in these sensitivity analyses  
 563 and only for some carbon-dioxide-based products.

564 Comparing different case studies, a lower overall environmental impact was obtained when additional  
 565 methanol was produced. On the other hand, the highest GWP value was obtained with wheat production.  
 566 The higher environmental impact in terms of GWP at a higher utilization rate of carbon dioxide was due to  
 567 a higher specific environmental impact for the utilization processes compared to that of the storage system.  
 568 This result was in agreement with the work of Cuellar-Franca and Azapagic (2015), where a comparison  
 569 between CCS and CCU was presented: on average, the GWP for CCS is significantly lower than that for the  
 570 CCU option. For example, for biodiesel production, the GWP is four times higher than that for CCS, while  
 571 the carbon mineralization and the EOR have a GWP that is 2.9 and 1.8 times higher than that for CCS,  
 572 respectively. Then, even if the utilization solution produces a better economic return helps to reduce costs  
 573 because of the profit generated (a better economic potential is ensured), it has an overall environmental impact  
 574 in terms of higher GWP compared to storage is higher.

575 As a result, this demonstrates that the storage section is important and should be designed at the optimal  
 576 operating conditions. Also, the storage is important because the demand for chemicals and other products  
 577 does not have the capacity to sink enough carbon dioxide emissions to achieve the carbon reduction targets  
 578 (Cuellar-Franca and Azapagic, 2015). It was estimated that the annual production of urea and methanol  
 579 requires only 0.5% of the current 34.5 Gtonne/year of the anthropogenic global carbon dioxide emissions

Commentato [BD44]: what was it? If it was for all just delete it.  
 Commentato [GL45R44]: Ok, I deleted it.



580 (ISPRA, 2013). The same ~~consideration-conclusion~~ about the importance of carbon storage was reported by  
581 Aldaco et al. (2019) comparing a CCU with a CCS system.

582 For the other impact categories (~~those~~ considered here in the LCA and sensitivity analyses; in addition to  
583 GWP), a comparison with the literature can ~~not hardly~~ be performed because a complete LCA, i.e. including  
584 the additional impact categories, was not yet developed in previous studies for CCUS supply chains. ~~given~~  
585 ~~the utilization of technologies only recently assessed. In fact,~~ Cuellar-Franca and Azapagic (2015) suggested  
586 ~~that, for future works, to consider~~ a wider range of LCA impacts ~~be considered in future~~, rather than focusing  
587 ~~only~~ on the GWP ~~only, and as well as~~ to examine ~~the~~ various utilization options of carbon dioxide; as ~~has been~~  
588 done for the supply chains ~~developed~~ here. ~~However, as Table 16 shows and as discussed above some impact~~  
589 ~~categories are increasing other are decreasing or constant by raising the utilization rate of carbon dioxide when~~  
590 ~~different products are obtained.~~

591

592 ~~As shown in Table 13, increasing the amount of methanol production and reducing that of carbon dioxide~~  
593 ~~stored did not affect the values for of AP, EP, ODP, MAETP and POCP, while it increased the value of ADP~~  
594 ~~elements and FAETP. On the other hand, ADP fossil, HTP and TETP decreased. Whereith concrete curing~~  
595 ~~getting bigger becomes greater at the expense of the amount of carbon dioxide stored, the values of AP, EP and~~  
596 ~~POCP increased, while the values of ODP, ADP elements and MAETP remained constant. A decrement~~  
597 ~~decrease was registered obtained for ADP fossil and FAETP. When more urea was produced utilizing carbon~~  
598 ~~dioxide that should have been stored, results showed that the value of AP, EP, ODP, ADP elements, ADP~~  
599 ~~fossil, HTP and POCP increased, while MAETP and TETP were kept constant. On the other hand, only FAETP~~  
600 ~~decreased. When more wheat was produced while reducing the amount of carbon dioxide stored, as shown in~~  
601 ~~Table 13, the value of AP, EP, ODP, ADP elements, MAETP and POCP were constant. A negative trend was~~  
602 ~~registered for ADP fossil, FAETP, HTP and TETP. When more lignin was treated with carbon dioxide that~~  
603 ~~should have been stored, most of impact categories had a positive trend (AP, ODP, ADP elements, ADP fossil,~~  
604 ~~HTP, MAETP and POCP). A constant trend was obtained for EP, FAETP and TETP. More polyurethane was~~  
605 ~~produced at a higher utilization rate of carbon dioxide: it resulted that all impact categories were increasing.~~  
606 ~~On the other hand, considering the effect to increase calcium carbonate production, the value of AP, ADP~~  
607 ~~elements, HTP, MAETP, POCP and TETP increased. A negative effect was obtained for ADP fossil, while a~~  
608 ~~constant value was registered for EP, ODP and FAETP. Increasing the utilization rate for concrete production~~  
609 ~~by red mud had a positive effect on AP, EP, HTP, POCP and TETP. A negative effect was observed for ADP~~  
610 ~~fossil, while it was insignificant for ODP, ADP elements, FAETP and MAETP.~~

611 Although LCA ~~studies and respective~~ results for new utilization processes will undoubtedly evolve, LCA at  
612 this stage will help to provide suggestions for future ~~studies researches~~ aiming at higher energy efficiencies and  
613 ~~other~~ environmental advantages. With this in mind, an additional LCA study was carried out ~~considering~~  
614 ~~incorporating~~ a higher efficiency of methanol synthesis; in terms of global carbon dioxide conversion. ~~This,~~  
615 ~~that~~ should reduce carbon dioxide emissions at the outlet of the chemical reactor (Leonzio and Foscolo, 2020;

25

**Commentato [BD46]:** This is extremely difficult to read and just seems to reproduce the results in Table 13 which is not necessary. What are the key lessons to be learned from all of this? The paragraph should just concentrate on this not on the detail.

**Commentato [GL47R46]:** I just added that some impact categories are increasing, decreasing or constant at higher utilization rate of CO<sub>2</sub>. Then I deleted the section.

616 Leonzio et al., 2019). As defined before, the methanol reactor includes the recycle of unconverted gases, after  
 617 the separation of methanol and water, to improve carbon dioxide conversion ~~up to high values~~. Efficiencies  
 618 higher than that corresponding to 80% recycle (~~base case, mentioned used above in the base case~~) were  
 619 considered here, in order to study the effect of changing ~~the carbon dioxide conversion~~ to methanol ~~conversion~~  
 620 ~~rate~~ on the ~~various~~ impact categories of ~~the~~ LCA, ~~at for~~ different utilization and storage rates of CO<sub>2</sub>. Results  
 621 of this sensitivity analysis are shown qualitatively in Table 17 (~~the corresponding~~, exact values are reported in  
 622 Tables S11 and S12).

623 Table 17 Results of sensitivity analysis when increasing carbon dioxide utilization rate, at different ~~rates of~~  
 624 carbon dioxide conversion to methanol; arrows indicate variation of each impact category with reference to  
 625 the base case (↔ constant value; ↑/↓ low variation (< 5%) upwards/downwards).

| CO <sub>2</sub> conversion | GWP | AP | EP | ODP steady state | ADP elements | ADP fossil | FAETP | HTP | MAETP | POCP | TETP |
|----------------------------|-----|----|----|------------------|--------------|------------|-------|-----|-------|------|------|
| 100%                       | ↔   | ↔  | ↔  | ↔                | ↑            | ↓          | ↑     | ↓   | ↔     | ↔    | ↓    |
| 90%                        | ↔   | ↔  | ↔  | ↔                | ↑            | ↓          | ↑     | ↓   | ↔     | ↔    | ↔    |

627  
 628 ~~The GWP remains constant~~ When increasing the utilization ratio of carbon dioxide ~~the GWP remains constant~~  
 629 for a fixed amount of captured carbon dioxide and for a defined carbon dioxide conversion. On the other hand,  
 630 for a different ~~carbon dioxide conversion rate level to methanol, we performed the same sensitivity~~ analysis  
 631 ~~resulting from~~ increasing the utilization rate of carbon dioxide to methanol ~~produces~~ a different value of GWP  
 632 ~~was obtained~~ with respect to the base case.

633 ~~In any case, w~~ When global carbon dioxide conversion of methanol synthesis is fixed at 90%, ADP elements  
 634 and FAETP increased, while ADP fossil and HTP decreased. When global carbon dioxide conversion is  
 635 approaching 100%, ~~also~~ TETP ~~also~~ decreased, suggesting a lower environmental impact.

636 ~~It was shown~~ These results show that improving the efficiency of the methanol process allows ~~to send~~ a higher  
 637 amount of carbon dioxide ~~to be sent~~ to the utilization section and ~~to reduce~~ that sent to the storage section ~~to~~  
 638 ~~be reduced~~ without increasing the value of GWP, ~~compared to the base case~~. However, it is difficult to  
 639 ~~operate/realize~~ a methanol process based on carbon dioxide hydrogenation with these high efficiencies, ~~and~~  
 640 ~~further research investigations would be needed to this aim, with environmental and energetic advantages.~~  
 641 However this result indicates that research towards increased methanol conversion rates would produce  
 642 environmental and energetic advantages for CCUS.-

#### 643 4.2 Interpretation phase for the ~~Italian~~ CCUS supply chain ~~of Italy~~

644 ~~The previous/Previous~~ results suggested that ~~significant issues/hotspots (processes with a higher environmental~~  
 645 ~~impact)~~ were linked to CO<sub>2</sub> sources, especially Puglia and Lombardy, where iron and steel plants are present.

646 As for the ~~previous-German~~ supply chain, a sensitivity analysis was ~~undertaken/developed~~ keeping constant  
 647 the amount of captured carbon dioxide, while increasing the amount of emissions utilized for methane  
 648 production and reducing those sent to storage. 25%, 50%, 75% of ~~base case values for~~ carbon dioxide sent to  
 649 storage section ~~in the base case was stored were used~~ in this analysis. ~~The remainder and the rest~~ was used for  
 650 methane production. The amount of methane ~~that was~~ produced ~~in the respective case study~~ was ~~of- in the~~

Commentato [BD48]: What does this mean? What issues? How linked to 'CO2 sources'? Also this needs a reference

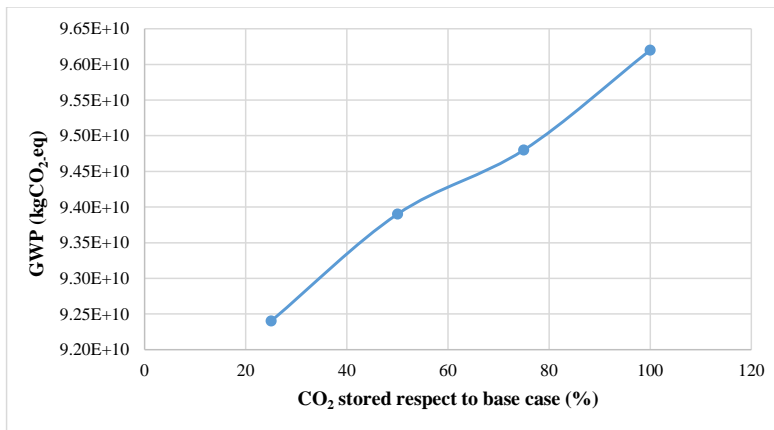
Commentato [GL49R48]: With issue I mean the hotspot, processes with a higher environmental impact.

651 three sensitivity cases were 25 Mtonne/year, 22 Mtonne/year and 19 Mtonne/year. In the base case, 16.1  
652 Mtonne/year of methane were produced. Results showed that ~~the GWP was reduced~~, when an increasing  
653 amount of carbon dioxide is sent to the utilization section ~~the GWP was reduced~~. ~~Then, f~~ For ~~the~~ Italian  
654 supply chain ~~in Italy~~, utilization is preferred over storage because a lower GWP can be obtained, as shown in  
655 Figure 5 ~~and for this reason the~~.

656 ~~The~~ GWP ~~the environmental impact~~ associated ~~to~~with carbon dioxide storage by injection in the saline aquifer is  
657 higher than that of methane ~~production~~. This may be explained by the noticeable utilization of ~~green~~ hydrogen  
658 ~~together with CO<sub>2</sub>~~ in the synthesis of methane, ~~together with CO<sub>2</sub>~~ (at a molar ratio of ~~=~~ 4:1).

Commentato [BD50]: This is unclear. For all impact measures?

Commentato [GL51R50]: I explained it better!



659

660 Figure 5 GWP as a function of different percentages of carbon dioxide sent to storage, with respect to the base  
661 case, when additional methane is produced in the ~~Italian~~ CCUS supply chain ~~of Italy~~.

662

663 The trend for the other impact categories obtained ~~when~~ increasing the utilization rate of carbon dioxide, ~~(still~~  
664 ~~keeping constant the amount captured)~~, is shown in Table 18 (the exact values are reported in Table S13).  
665 Overall, a lower environmental impact was obtained, because all impact categories were reduced, except  
666 ~~the~~for EP that ~~was~~remained constant. In this case, storage was ~~an unfavorable option for~~ ~~to~~reducin~~g~~e the  
667 environmental impact. These results suggest~~ed~~ that ~~the~~ power to gas technology is a ~~process~~ cleaner and more  
668 environmentally friendly ~~process~~ than the storage option ~~with~~and other utilization systems ~~which was the~~  
669 ~~conclusion for the German case~~(evaluated for the CCUS supply chain in Germany). ~~In fact, a~~ No carbon  
670 dioxide emissions were present at the outlet of the chemical reactor. Carbon dioxide conversion and methane  
671 selectivity ~~can~~ reach values close to 100%, especially under stoichiometric conditions (Stangeland et al., 2015).

672

673

674 **Table 18** Results of the sensitivity analysis regarding different impact categories when higher fractions of CO<sub>2</sub>  
 675 flow rate are utilized for methane production; arrows indicate variations with respect to the base case (↔  
 676 constant value, ↓/↗ low variation (<5%), ↓/↗ medium variation (<50%))

| GWP | AP | EP | ODP steady state | ADP elements | ADP fossil | FAETP | MAETP | POCP | TETP |
|-----|----|----|------------------|--------------|------------|-------|-------|------|------|
| ↓   | ↓  | ↔  | ↓                | ↓            | ↓          | ↓     | ↓     | ↓    | ↓    |

677

678

### 679 4.3 Comparison and further discussion about the CCUS supply chains

680 ~~For the CCUS supply chain in Germany (Leonzio et al., 2019), carbon dioxide was used to produce methanol,~~  
 681 ~~urea, concrete, polyurethane, calcium carbonate, wheat and for lignin treatment. Considering these processes~~  
 682 ~~from an environmental point of view, it was found in the above~~The sensitivity analysis (in section 4.1) showed  
 683 that storage is preferred over utilization. For the Italian CCUS supply chain in Italy (Leonzio and Zondervan,  
 684 2020), carbon dioxide was used to produce methane in a power to gas system. In this case, utilization is  
 685 preferred over storage to ~~get reduce~~ a lower the environmental impact, as found in the previous sensitivity  
 686 analysis (section 4.2). ~~Then, t~~ These results suggest that the best carbon dioxide utilization system is the power  
 687 to gas system. Sternberg and Bardow (2016) suggested that for power-to-gas the global warming impact is  
 688 about 0.222 kg CO<sub>2-eq</sub>/FU<sub>SNG</sub> while the fossil depletion impact is 0.072 kg Oil<sub>eq</sub>/FU<sub>SNG</sub> in 2020.  
 689 ~~Our results confirm that t~~his last technology is the most effective and mature process that avoids ~~ante~~ increase  
 690 in the environmental impact ~~with its for CO2 utilization. Even if the~~While power to gas systems ~~is are~~ expected  
 691 to have an important role in the energy transition, ~~there are~~ only few ~~studies works are dealing with reporting~~  
 692 a LCA ~~effor~~ for this technology (Gotz et al., 2016; Meylana et al., 2017; Sternberg and Bardow, 2015).

693

### 694 5. Conclusions

695 In this ~~research study,~~ a Life Cycle Analysis was carried out for large scale CCUS supply chains developed in  
 696 previous studies for Germany and Italy (Leonzio et al., 2019; Leonzio and Zondervan 2020). ~~Compared to the~~  
 697 ~~existing literature, not yet investigated~~ carbon dioxide based products were taken into account for this  
 698 environmental analysis. This study particularly incorporated the utilization of CO<sub>2</sub> through the chemical  
 699 conversion to a range of useful products.

700 The LCA results for Germany showed that it was possible to reduce German carbon dioxide emissions through  
 701 storage and utilization to 640 Mton<sub>ne</sub>. This is a value lower than the target set by the European environmental  
 702 policy for Germany ~~demonstrating the power of this approach.~~

703

704 A sensitivity analysis showed that storage is more effective in reducing the value of GWP than additional  
 705 utilization of carbon dioxide to ~~obtain~~produce useful products. Other impact categories remained constant or  
 706 in some cases worsened.

Formattato: SpazioDopo: 0 pt

Commentato [DB52]: What does this mean?

Commentato [GL53R52]: That are interesting, but I changed it.

707 The LCA results for Italy showed that total carbon emissions for Italy ~~were predicted to~~ could be reduced to  
708 249 Mtonne, a value below that required by the national environmental policies. A sensitivity analysis showed  
709 that the value of GWP was reduced if additional carbon dioxide was used to produce methane instead of being  
710 stored, keeping constant the overall quantity of CO<sub>2</sub> captured, while other indicators of impact categories  
711 decreased or remained constant. This result suggests that for the Italian CCUS supply chain ~~of Italy~~ storage is  
712 less important to reduce the value of GWP, ~~in comparison to and that the~~ power to gas system, ~~has more~~  
713 ~~beneficial results in this case, that~~ is a more environmentally friendly process than the storage and the other  
714 ~~utilization options considered in the CCUS supply chain of Germany.~~ The power to gas system is predicted to  
715 be the most realistic beneficial and mature process that to avoids an increase in the environmental impact ~~with~~  
716 ~~its utilization.~~ It is also a more mature technology.

717 This work shows ~~that inside a carbon supply chain how using LCA and sensitivity analysis it is possible to~~  
718 ~~helps find systems that~~ increase the utilization rate of carbon dioxide ~~with while also~~ reductioning, or at least  
719 ~~keeping constant, of the~~ GWP, ~~or at least keeping it constant, with a reduction of +~~ The indicators ~~of~~ other  
720 impact categories are reduced only when the power to gas process is ~~used forehosen to utilize~~ carbon dioxide  
721 utilization. Additional studies are ~~therefore~~ recommended in order to develop ~~ever~~ more sustainable processes  
722 for power to gas, ~~particularly~~ to obtain a reduction of GWP even at high methane production rates.

723 ~~Moreover, f~~ Further studies and developments are needed ~~should be conducted~~ to improve the overall  
724 environmental burden of new carbon dioxide utilization routes, ~~with the aim in order~~ to make them  
725 environmentally preferable ~~over the to~~ storage at higher utilization rates. ~~The if~~ Further improvement of  
726 conversion efficiencies ~~and reduction of fossil fuel raw materials should be considered. This would~~ allow a  
727 wider choice ~~from~~ among the various carbon dioxide utilization options. ~~This would~~ contribute ~~ing~~ further to  
728 the reduction of emissions ~~compared to over~~ the case when only methane production is the preferred route. This  
729 also agrees with the ~~principle of~~ circular economy principles, ~~based on the recovery of a waste as carbon~~  
730 ~~dioxide to produce different valuable products. , although additional research is required for its application.~~  
731 In addition, increasing carbon dioxide utilization options could reduce the overall cost ~~of the framework by~~  
732 ~~m~~by increasing revenues ~~helping the spread of these technologies. Nevertheless, m~~ More studies are needed  
733 to develop more environmentally friendly utilization routes, ~~so that carbon dioxide storage has still in most~~  
734 ~~eases an important role to achieve a reduction of the overall environmental impact according to the well defined~~  
735 ~~targets set by International Agreements.~~ A trade-off between carbon dioxide storage and utilization is currently  
736 required ~~and this needs thorough exploration in each case.~~

737  
738 In a future study, it would be also interesting to analyze the same supply chains with different carbon dioxide  
739 sources, for example with carbon dioxide captured from ambient air.

Commentato [DB54]: I don't understand what this means.

Commentato [GL55R54]: Cleaner=more environmental friendly

Commentato [BD56]: How?

Commentato [GL57R56]: I explained it.

Commentato [BD58]: Not significant.

Commentato [GL59R58]: This sentence was suggested by the reviewer.

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748 **Declarations**

749 Not applicable

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751 **Acknowledgment**

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753 grant to spend a six months research period at the University College London, UK.

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990 **Supplementary Materials**

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992 **1. Life cycle inventory phase**

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994 **Table S1**

995 Results of LCIA analysis for the CCUS supply chain of Germany

|                  |                       |                           |
|------------------|-----------------------|---------------------------|
| AP               | $1.57 \times 10^9$    | kgSO <sub>2eq</sub>       |
| EP               | $3.04 \times 10^{10}$ | kgPhosphate <sub>eq</sub> |
| ODP steady state | $3.76 \times 10^3$    | kgR11 <sub>eq</sub>       |
| ADP elements     | $4.25 \times 10^5$    | kgSb <sub>eq</sub>        |
| ADP fossil       | $3.44 \times 10^{12}$ | MJ                        |
| FAETP            | $7.43 \times 10^{10}$ | kgDCB <sub>eq</sub>       |
| HTP              | $5.27 \times 10^{10}$ | kgDCB <sub>eq</sub>       |
| MAETP            | $4.54 \times 10^{14}$ | kgDCB <sub>eq</sub>       |
| POCP             | $1.84 \times 10^8$    | kgethene <sub>eq</sub>    |
| TETP             | $1.49 \times 10^9$    | kgDCB <sub>eq</sub>       |

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998 **Table S2**

999 Results for different impact categories, considered in the LCIA analysis for the CCUS supply chain in Italy

|                  |                       |                           |
|------------------|-----------------------|---------------------------|
| AP               | $4.67 \times 10^8$    | kgSO <sub>2eq</sub>       |
| EP               | $1.15 \times 10^{11}$ | kgPhosphate <sub>eq</sub> |
| ODP steady state | 368                   | kgR11 <sub>eq</sub>       |
| ADP elements     | $2.27 \times 10^4$    | kgSb <sub>eq</sub>        |
| ADP fossil       | $1.96 \times 10^{12}$ | MJ                        |
| FAETP            | $9.27 \times 10^{10}$ | kgDCB <sub>eq</sub>       |
| MAETP            | $1.02 \times 10^{13}$ | kgDCB <sub>eq</sub>       |
| POCP             | $7.88 \times 10^7$    | kgethene <sub>eq</sub>    |
| TETP             | $4.42 \times 10^7$    | kgDCB <sub>eq</sub>       |

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1003 **2. Results of sensitivity analysis**1004 **2.1 CCUS of Germany**

1005 Assuming that the fraction of carbon dioxide sent to the utilization section is used to produce methanol, and  
 1006 the captured carbon dioxide is stored at a rate of only 25%, 50%, 75% of the base case, the calculated methanol  
 1007 production is 9.8 Mton/year, 6.8 Mton/year and 3.8 Mton/year, respectively. Keeping constant the amount of  
 1008 captured carbon dioxide, and reducing the amount of carbon dioxide sent to storage (i.e. producing more

1009 methanol), the AP, EP, ODP, MAETP, POCP remain constant. On the other hand, the GWP, ADP elements  
1010 and FAETP fossil increase compared to the base case. However, the GWP increases only slightly compared to  
1011 base case. The opposite trend is observed for the ADP fossil, HTP and TETP. Overall, the variation of these  
1012 impact categories is not significant compared to the base case.

1013 In the following analysis, carbon dioxide that is not stored is utilized for concrete curing: when the stored  
1014 amount of carbon dioxide is only 25%, 50%, 75% of the base case, CO<sub>2</sub>-cured concrete is 513 Mton/year, 343  
1015 Mton/year and 174 Mton/year, respectively. Results show that for the ODP, ADP elements and MAETP no  
1016 variations are present. The GWP, AP, EP, HTP, POCP, TETP are increased, then a higher environmental  
1017 impact is present, especially for the POCP. The highest value that is achieved for the GWP is  $3.46 \cdot 10^{11}$  kgCO<sub>2</sub>-  
1018 eq, when carbon dioxide stored is only 25% of the base case. Reductions are present for the FAETP and ADP  
1019 fossil. Overall, producing a higher amount of CO<sub>2</sub>-cured concrete increases the environmental impact.

1020 In the following analysis, carbon dioxide that is not stored is used to produce urea. When stored carbon dioxide  
1021 is only 25%, 50%, 75% of the base case, urea production is of 21.9 Mton/year, 15.5 Mton/year and 8.2  
1022 Mton/year, respectively. Results show that the TETP and MAETP have a constant trend, while the GWP, AP,  
1023 EP, ADP fossil, HTP and POCP increase. The highest value for GWP is  $2.28 \cdot 10^{11}$  kgCO<sub>2</sub>-eq. On the other hand,  
1024 only the FAETP is reduced increasing carbon dioxide sent to the utilization section. Overall, like in the  
1025 previous case, the increase of urea production is not favorable to the reduction of the environmental impact.

1026 Carbon dioxide that is not stored is sent to the utilization section to produce wheat. The total CO<sub>2</sub>-assisted  
1027 production of wheat, when carbon dioxide stored is only 25%, 50% and 75% of that sent to the storage section  
1028 in the base case, is respectively  $3.05 \cdot 10^{10}$  ton/year,  $2.03 \cdot 10^{10}$  ton/year and  $1.02 \cdot 10^{10}$  ton/year. With an  
1029 increasing amount of carbon dioxide utilized for wheat production, only the GWP increases and a higher value  
1030 compared to the base case is obtained ( $8.55 \cdot 10^{12}$  kgCO<sub>2</sub>-eq compared to  $1.94 \cdot 10^{11}$  kgCO<sub>2</sub>-eq of the base case).  
1031 This suggests a higher environmental impact, even if a reduction of ADP fossil, FAETP, HTP and TETP is  
1032 predicted. The other impact categories like POCP, MAETP, ADP elements, ODP, EP and AP present a  
1033 constant trend.

1034 Carbon dioxide not stored is sent to the utilization for lignin treatment: when only 25%, 50% and 75% of  
1035 carbon dioxide sent to the storage section in the base case is stored, the respective amount of lignin that is  
1036 upgraded is 69.7 Mton/year, 46.6 Mton/year and 23.5 Mton/year. Overall, increasing the lignin that is treated  
1037 determines a higher environmental impact. In fact, the GWP, AP, ODP, ADP elements, ADP fossil, HTP,  
1038 MAETP and POCP increase. However, as in the methanol case, no significant variations are obtained. For  
1039 example, the highest value of GWP is  $2.06 \cdot 10^{11}$  kgCO<sub>2</sub>-eq. On the other hand, the TETP and FAETP show no  
1040 variation.

1041 When increasing the amount of carbon dioxide sent to the utilization for polyurethane production, it is evident  
1042 that the environmental impact increases. The highest variation compared to the base case is present for the  
1043 ADP elements, while for the other impact categories no significant variations compared to the base case are

1044 obtained. The highest GWP is  $2.88 \cdot 10^{11}$  kgCO<sub>2-eq</sub>. When only 25%, 50% and 75% of carbon dioxide sent to  
 1045 storage section in the base case is stored, the amount of polyurethane that is produced is respectively 62  
 1046 Mton/year, 45 Mton/year and 28 Mton/year. Polyurethane is obtained in a conventional way by polyols and  
 1047 isocyanate, however it should be stressed here that we are not considering the traditional route for polyols  
 1048 production. These are obtained from carbon dioxide: CO<sub>2</sub> reacts with epoxides to produce polycarbonate  
 1049 polyols via a catalytic reaction (Orgilés-Calpena et al., 2016). The mechanical properties of resulting  
 1050 polyurethane are comparable with those obtained through a traditional way (Orgilés-Calpena et al., 2016).

1051 In the following sensitivity analysis, the amount of carbon dioxide that is not stored is sent to the utilization  
 1052 for the production of calcium carbonate. When only 25%, 50%, 75% of carbon dioxide sent to the storage  
 1053 section in the base case is stored, the amount of calcium carbonate that is produced is respectively 135  
 1054 Mton/year, 131 Mton/year and 126 Mton/year. A constant trend is present for the EP, ODP and FAETP.  
 1055 Increasing the utilization option, a reduction is obtained only for the ADP fossil, while an increment is obtained  
 1056 for other impact categories. The highest value for GWP is  $1.96 \cdot 10^{11}$  kgCO<sub>2-eq</sub>. However, no significant  
 1057 variations compared to base case are present.

1058 In the last sensitivity analysis, carbon dioxide not stored is sent to utilization for the production of concrete by  
 1059 red mud. When only 25%, 50% and 75% of carbon dioxide sent to the storage in the base case is actually  
 1060 stored, the amount of concrete produced is respectively 1.16 billion ton/year, 783 Mton/year and 401  
 1061 Mton/year. A constant trend is present for the ODP, ADP elements, FAETP and MAETP. Generally, increasing  
 1062 the amount of carbon dioxide sent to the utilization section, the GWP, AP, EP, HTP, POCP and TETP increase,  
 1063 while only the ADP fossil decreases. The highest value of GWP is  $5.79 \cdot 10^{11}$  kgCO<sub>2-eq</sub>, calculated when only  
 1064 25% of carbon dioxide is stored in storage section compared to the base case. However, no substantial  
 1065 variations are predicted compared to base case for these impact categories.

1066 The following Tables S3 – S10 summarize the results obtained with the sensitivity analysis for the CCUS of  
 1067 Germany, with reference to different scenarios (see also the methodology applied in Xiang et al. (2015)

1068 Table S3 Results of sensitivity analysis considering methanol production for the CCUS of Germany

|                                    | Base case (A) | 25% CO <sub>2</sub> stored<br>compared A | 50% CO <sub>2</sub> stored<br>compared A | 75% CO <sub>2</sub> stored<br>compared A |
|------------------------------------|---------------|--|--|--|
| GWP (kgCO <sub>2eq</sub> )         | 1.94E+11      | 1.98E+11                                 | 1.97E+11                                 | 1.95E+11                                 |
| AP (kgSO <sub>2eq</sub> )          | 1.57E+09      | 1.57E+09                                 | 1.57E+09                                 | 1.57E+09                                 |
| EP (kgPhosphate <sub>eq</sub> )    | 3.04E+10      | 3.04E+10                                 | 3.04E+10                                 | 3.04E+10                                 |
| ODP (kgR11 <sub>eq</sub> )         | 3.76E+03      | 3.76E+03                                 | 3.76E+03                                 | 3.76E+03                                 |
| ADP elements (kgSb <sub>eq</sub> ) | 4.25E+05      | 4.28E+05                                 | 4.27E+05                                 | 4.26E+05                                 |
| ADP fossil (MJ)                    | 3.44E+12      | 3.39E+12                                 | 3.40E+12                                 | 3.42E+12                                 |
| FAETP (kgDCB <sub>eq</sub> )       | 7.43E+10      | 7.48E+10                                 | 7.46E+10                                 | 7.44E+10                                 |
| HTP inf (kgDCB <sub>eq</sub> )     | 5.27E+10      | 5.25E+10                                 | 5.26E+10                                 | 5.26E+10                                 |
| MAETP (kgDCB <sub>eq</sub> )       | 4.54E+14      | 4.54E+14                                 | 4.54E+14                                 | 4.54E+14                                 |
| POCP (kgethene <sub>eq</sub> )     | 1.84E+08      | 1.84E+08                                 | 1.84E+08                                 | 1.84E+08                                 |
| TETP (kgDCB <sub>eq</sub> )        | 1.49E+09      | 1.48E+09                                 | 1.49E+09                                 | 1.49E+09                                 |

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1070 Table S4 Results of sensitivity analysis considering concrete curing for the CCUS of Germany

|                                    | Base case (A) | 25% CO <sub>2</sub> stored<br>compared A | 50% CO <sub>2</sub> stored<br>compared A | 75% CO <sub>2</sub> stored<br>compared A |
|------------------------------------|---------------|--|--|--|
| GWP (kgCO <sub>2eq</sub> )         | 1.94E+11      | 3.46E+11                                 | 2.95E+11                                 | 2.45E+11                                 |
| AP (kgSO <sub>2eq</sub> )          | 1.57E+09      | 2.43E+09                                 | 2.15E+09                                 | 1.86E+09                                 |
| EP (kgPhosphate <sub>eq</sub> )    | 3.04E+10      | 3.05E+10                                 | 3.05E+10                                 | 3.04E+10                                 |
| ODP (kgR11 <sub>eq</sub> )         | 3.76E+03      | 3.76E+03                                 | 3.76E+03                                 | 3.76E+03                                 |
| ADP elements (kgSb <sub>eq</sub> ) | 4.25E+05      | 4.25E+05                                 | 4.25E+05                                 | 4.25E+05                                 |
| ADP fossil (MJ)                    | 3.44E+12      | 3.38E+12                                 | 3.40E+12                                 | 3.42E+12                                 |
| FAETP (kgDCB <sub>eq</sub> )       | 7.43E+10      | 7.42E+10                                 | 7.42E+10                                 | 7.42E+10                                 |
| HTP inf (kgDCB <sub>eq</sub> )     | 5.27E+10      | 5.56E+10                                 | 5.46E+10                                 | 5.37E+10                                 |
| MAETP (kgDCB <sub>eq</sub> )       | 4.54E+14      | 4.54E+14                                 | 4.54E+14                                 | 4.54E+14                                 |
| POCP (kgethene <sub>eq</sub> )     | 1.84E+08      | 1.12E+09                                 | 8.11E+08                                 | 4.98E+08                                 |
| TETP (kgDCB <sub>eq</sub> )        | 1.49E+09      | 1.57E+09                                 | 1.54E+09                                 | 1.52E+09                                 |

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1074 Table S5 Results of sensitivity analysis considering urea production for the CCUS of Germany

|                                    | Base case (A) | 25% CO <sub>2</sub> stored<br>compared A | 50% CO <sub>2</sub> stored<br>compared A | 75% CO <sub>2</sub> stored<br>compared A |
|------------------------------------|---------------|--|--|--|
| GWP (kgCO <sub>2eq</sub> )         | 1.94E+11      | 2.28E+11                                 | 2.16E+11                                 | 2.05E+11                                 |
| AP (kgSO <sub>2eq</sub> )          | 1.57E+09      | 1.72E+09                                 | 1.67E+09                                 | 1.62E+09                                 |
| EP (kgPhosphate <sub>eq</sub> )    | 3.04E+10      | 3.07E+10                                 | 3.06E+10                                 | 3.05E+10                                 |
| ODP (kgR11 <sub>eq</sub> )         | 3.76E+03      | 3.77E+03                                 | 3.76E+03                                 | 3.76E+03                                 |
| ADP elements (kgSb <sub>eq</sub> ) | 4.25E+05      | 4.28E+05                                 | 4.27E+05                                 | 4.26E+05                                 |
| ADP fossil (MJ)                    | 3.44E+12      | 3.80E+12                                 | 3.68E+12                                 | 3.56E+12                                 |
| FAETP (kgDCB <sub>eq</sub> )       | 7.43E+10      | 7.42E+10                                 | 7.42E+10                                 | 7.42E+10                                 |
| HTP inf (kgDCB <sub>eq</sub> )     | 5.27E+10      | 5.28E+10                                 | 5.28E+10                                 | 5.27E+10                                 |
| MAETP (kgDCB <sub>eq</sub> )       | 4.54E+14      | 4.54E+14                                 | 4.54E+14                                 | 4.54E+14                                 |
| POCP (kgethene <sub>eq</sub> )     | 1.84E+08      | 1.86E+08                                 | 1.85E+08                                 | 1.85E+08                                 |
| TETP (kgDCB <sub>eq</sub> )        | 1.49E+09      | 1.49E+09                                 | 1.49E+09                                 | 1.49E+09                                 |

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1082 Table S6 Results of sensitivity analysis considering wheat production for the CCUS of Germany

|                                    | Base case (A) | 25% CO <sub>2</sub> stored<br>compared A | 50% CO <sub>2</sub> stored<br>compared A | 75% CO <sub>2</sub> stored<br>compared A |
|------------------------------------|---------------|--|--|--|
| GWP (kgCO <sub>2eq</sub> )         | 1.94E+11      | 8.55E+12                                 | 5.77E+12                                 | 2.98E+12                                 |
| AP (kgSO <sub>2eq</sub> )          | 1.57E+09      | 1.57E+09                                 | 1.57E+09                                 | 1.57E+09                                 |
| EP (kgPhosphate <sub>eq</sub> )    | 3.04E+10      | 3.04E+10                                 | 3.04E+10                                 | 3.04E+10                                 |
| ODP (kgR11 <sub>eq</sub> )         | 3.76E+03      | 3.76E+03                                 | 3.76E+03                                 | 3.76E+03                                 |
| ADP elements (kgSb <sub>eq</sub> ) | 4.25E+05      | 4.25E+05                                 | 4.25E+05                                 | 4.25E+05                                 |
| ADP fossil (MJ)                    | 3.44E+12      | 3.38E+12                                 | 3.40E+12                                 | 3.42E+12                                 |
| FAETP (kgDCB <sub>eq</sub> )       | 7.43E+10      | 7.42E+10                                 | 7.42E+10                                 | 7.42E+10                                 |
| HTP inf (kgDCB <sub>eq</sub> )     | 5.27E+10      | 5.25E+10                                 | 5.26E+10                                 | 5.26E+10                                 |
| MAETP (kgDCB <sub>eq</sub> )       | 4.54E+14      | 4.54E+14                                 | 4.54E+14                                 | 4.54E+14                                 |
| POCP (kgethene <sub>eq</sub> )     | 1.84E+08      | 1.84E+08                                 | 1.84E+08                                 | 1.84E+08                                 |
| TETP (kgDCB <sub>eq</sub> )        | 1.49E+09      | 1.48E+09                                 | 1.49E+09                                 | 1.49E+09                                 |

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1085 Table S7 Results of sensitivity analysis considering lignin production for the CCUS of Germany

|                                    | Base case (A) | 25% CO <sub>2</sub> stored<br>compared A | 50% CO <sub>2</sub> stored<br>compared A | 75% CO <sub>2</sub> stored<br>compared A |
|------------------------------------|---------------|--|--|--|
| GWP (kgCO <sub>2eq</sub> )         | 1.94E+11      | 2.06E+11                                 | 2.02E+11                                 | 1.98E+11                                 |
| AP (kgSO <sub>2eq</sub> )          | 1.57E+09      | 1.64E+09                                 | 1.62E+09                                 | 1.60E+09                                 |
| EP (kgPhosphate <sub>eq</sub> )    | 3.04E+10      | 3.04E+10                                 | 3.04E+10                                 | 3.04E+10                                 |
| ODP (kgR11 <sub>eq</sub> )         | 3.76E+03      | 3.77E+03                                 | 3.77E+03                                 | 3.76E+03                                 |
| ADP elements (kgSb <sub>eq</sub> ) | 4.25E+05      | 5.18E+05                                 | 4.87E+05                                 | 4.56E+05                                 |
| ADP fossil (MJ)                    | 3.44E+12      | 4.96E+12                                 | 4.45E+12                                 | 3.95E+12                                 |
| FAETP (kgDCB <sub>eq</sub> )       | 7.43E+10      | 7.43E+10                                 | 7.43E+10                                 | 7.43E+10                                 |
| HTP inf (kgDCB <sub>eq</sub> )     | 5.27E+10      | 5.30E+10                                 | 5.29E+10                                 | 5.28E+10                                 |
| MAETP (kgDCB <sub>eq</sub> )       | 4.54E+14      | 4.55E+14                                 | 4.54E+14                                 | 4.54E+14                                 |
| POCP (kgethene <sub>eq</sub> )     | 1.84E+08      | 1.88E+08                                 | 1.86E+08                                 | 1.85E+08                                 |
| TETP (kgDCB <sub>eq</sub> )        | 1.49E+09      | 1.49E+09                                 | 1.49E+09                                 | 1.49E+09                                 |

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1093 Table S8 Results of sensitivity analysis considering polyurethane production for the CCUS of Germany

|                                    | Base case (A) | 25% CO <sub>2</sub> stored compared A | 50% CO <sub>2</sub> stored compared A | 75% CO <sub>2</sub> stored compared A |
|------------------------------------|---------------|---------------------------------------|---------------------------------------|---------------------------------------|
| GWP (kgCO <sub>2eq</sub> )         | 1.94E+11      | 2.88E+11                              | 2.56E+11                              | 2.20E+11                              |
| AP (kgSO <sub>2eq</sub> )          | 1.57E+09      | 1.78E+09                              | 1.71E+09                              | 1.64E+09                              |
| EP (kgPhoshate <sub>eq</sub> )     | 3.04E+10      | 3.05E+10                              | 3.05E+10                              | 3.04E+10                              |
| ODP (kgR11 <sub>eq</sub> )         | 3.76E+03      | 3.96E+03                              | 3.89E+03                              | 3.82E+03                              |
| ADP elements (kgSb <sub>eq</sub> ) | 4.25E+05      | 1.50E+06                              | 1.14E+06                              | 7.81E+05                              |
| ADP fossil (MJ)                    | 3.44E+12      | 5.52E+12                              | 4.83E+12                              | 4.13E+12                              |
| FAETP (kgDCB <sub>eq</sub> )       | 7.43E+10      | 7.49E+10                              | 7.46E+10                              | 7.44E+10                              |
| HTP inf (kgDCB <sub>eq</sub> )     | 5.27E+10      | 8.12E+10                              | 7.17E+10                              | 6.22E+10                              |
| MAETP (kgDCB <sub>eq</sub> )       | 4.54E+14      | 4.60E+14                              | 4.58E+14                              | 4.56E+14                              |
| POCP (kgethene <sub>eq</sub> )     | 1.84E+08      | 2.07E+08                              | 1.99E+08                              | 1.91E+08                              |
| TETP (kgDCB <sub>eq</sub> )        | 1.49E+09      | 1.57E+09                              | 1.54E+09                              | 1.52E+09                              |

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1096 Table S9 Results of sensitivity analysis considering calcium carbonate production for the CCUS of Germany

|                                    | Base case (A) | 25% CO <sub>2</sub> stored compared A | 50% CO <sub>2</sub> stored compared A | 75% CO <sub>2</sub> stored compared A |
|------------------------------------|---------------|---------------------------------------|---------------------------------------|---------------------------------------|
| GWP (kgCO <sub>2eq</sub> )         | 1.94E+11      | 1.96E+11                              | 1.96E+11                              | 1.95E+11                              |
| AP (kgSO <sub>2eq</sub> )          | 1.57E+09      | 1.67E+09                              | 1.63E+09                              | 1.60E+09                              |
| EP (kgPhoshate <sub>eq</sub> )     | 3.04E+10      | 3.04E+10                              | 3.04E+10                              | 3.04E+10                              |
| ODP (kgR11 <sub>eq</sub> )         | 3.76E+03      | 3.76E+03                              | 3.76E+03                              | 3.76E+03                              |
| ADP elements (kgSb <sub>eq</sub> ) | 4.25E+05      | 4.30E+05                              | 4.28E+05                              | 4.27E+05                              |
| ADP fossil (MJ)                    | 3.44E+12      | 3.40E+12                              | 3.41E+12                              | 3.43E+12                              |
| FAETP (kgDCB <sub>eq</sub> )       | 7.43E+10      | 7.43E+10                              | 7.43E+10                              | 7.43E+10                              |
| HTP inf (kgDCB <sub>eq</sub> )     | 5.27E+10      | 5.65E+10                              | 5.52E+10                              | 5.40E+10                              |
| MAETP (kgDCB <sub>eq</sub> )       | 4.54E+14      | 5.03E+14                              | 4.87E+14                              | 4.71E+14                              |
| POCP (kgethene <sub>eq</sub> )     | 1.84E+08      | 1.90E+08                              | 1.88E+08                              | 1.86E+08                              |
| TETP (kgDCB <sub>eq</sub> )        | 1.49E+09      | 1.63E+09                              | 1.59E+09                              | 1.54E+09                              |

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1103 Table S10 Results of sensitivity analysis considering concrete production from red mud for the CCUS of  
 1104 Germany

|                                    | Base case (A) | 25% CO <sub>2</sub> stored compared A | 50% CO <sub>2</sub> stored compared A | 75% CO <sub>2</sub> stored compared A |
|------------------------------------|---------------|---------------------------------------|---------------------------------------|---------------------------------------|
| GWP (kgCO <sub>2eq</sub> )         | 1.94E+11      | 5.79E+11                              | 4.51E+11                              | 3.22E+11                              |
| AP (kgSO <sub>2eq</sub> )          | 1.57E+09      | 3.05E+09                              | 2.56E+09                              | 2.06E+09                              |
| EP (kgPhosphate <sub>eq</sub> )    | 3.04E+10      | 3.05E+10                              | 3.05E+10                              | 3.05E+10                              |
| ODP (kgR11 <sub>eq</sub> )         | 3.76E+03      | 3.76E+03                              | 3.76E+03                              | 3.76E+03                              |
| ADP elements (kgSb <sub>eq</sub> ) | 4.25E+05      | 4.25E+05                              | 4.25E+05                              | 4.25E+05                              |
| ADP fossil (MJ)                    | 3.44E+12      | 3.38E+12                              | 3.40E+12                              | 3.42E+12                              |
| FAETP (kgDCB <sub>eq</sub> )       | 7.43E+10      | 7.43E+10                              | 7.43E+10                              | 7.43E+10                              |
| HTP inf (kgDCB <sub>eq</sub> )     | 5.27E+10      | 5.91E+10                              | 5.69E+10                              | 5.48E+10                              |
| MAETP (kgDCB <sub>eq</sub> )       | 4.54E+14      | 4.54E+14                              | 4.54E+14                              | 4.54E+14                              |
| POCP (kgethene <sub>eq</sub> )     | 1.84E+08      | 1.86E+09                              | 1.30E+09                              | 7.41E+08                              |
| TETP (kgDCB <sub>eq</sub> )        | 1.49E+09      | 1.67E+09                              | 1.61E+09                              | 1.55E+09                              |

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1108 Table S11 Results of sensitivity analysis for methanol production with an efficiency of 90%

|                                    | Base case (A) | 25% CO <sub>2</sub> stored compared A | 50% CO <sub>2</sub> stored compared A | 75% CO <sub>2</sub> stored compared A |
|------------------------------------|---------------|---------------------------------------|---------------------------------------|---------------------------------------|
| GWP (kgCO <sub>2eq</sub> )         | 1.94E+11      | 1.94E+11                              | 1.94E+11                              | 1.94E+11                              |
| AP (kgSO <sub>2eq</sub> )          | 1.57E+09      | 1.57E+09                              | 1.57E+09                              | 1.57E+09                              |
| EP (kgPhosphate <sub>eq</sub> )    | 3.04E+10      | 3.04E+10                              | 3.04E+10                              | 3.04E+10                              |
| ODP (kgR11 <sub>eq</sub> )         | 3.76E+03      | 3.76E+03                              | 3.76E+03                              | 3.76E+03                              |
| ADP elements (kgSb <sub>eq</sub> ) | 4.25E+05      | 4.28E+05                              | 4.27E+05                              | 4.26E+05                              |
| ADP fossil (MJ)                    | 3.44E+12      | 3.39E+12                              | 3.40E+12                              | 3.42E+12                              |
| FAETP (kgDCB <sub>eq</sub> )       | 7.43E+10      | 7.48E+10                              | 7.46E+10                              | 7.44E+10                              |
| HTP inf (kgDCB <sub>eq</sub> )     | 5.27E+10      | 5.25E+10                              | 5.26E+10                              | 5.26E+10                              |
| MAETP (kgDCB <sub>eq</sub> )       | 4.54E+14      | 4.54E+14                              | 4.54E+14                              | 4.54E+14                              |
| POCP (kgethene <sub>eq</sub> )     | 1.84E+08      | 1.84E+08                              | 1.84E+08                              | 1.84E+08                              |
| TETP (kgDCB <sub>eq</sub> )        | 1.49E+09      | 1.48E+09                              | 1.49E+09                              | 1.49E+09                              |

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1114 Table S12 Results of sensitivity analysis for methanol production with an efficiency of 100%

|                                    | Base case (A) | 25% CO <sub>2</sub> stored compared A | 50% CO <sub>2</sub> stored compared A | 75% CO <sub>2</sub> stored compared A |
|------------------------------------|---------------|---------------------------------------|---------------------------------------|---------------------------------------|
| GWP (kgCO <sub>2eq</sub> )         | 1.94E+11      | 1.94E+11                              | 1.94E+11                              | 1.94E+11                              |
| AP (kgSO <sub>2eq</sub> )          | 1.57E+09      | 1.57E+09                              | 1.57E+09                              | 1.57E+09                              |
| EP (kgPhosphate <sub>eq</sub> )    | 3.04E+10      | 3.04E+10                              | 3.04E+10                              | 3.04E+10                              |
| ODP (kgR11 <sub>eq</sub> )         | 3.76E+03      | 3.76E+03                              | 3.76E+03                              | 3.76E+03                              |
| ADP elements (kgSb <sub>eq</sub> ) | 4.25E+05      | 4.28E+05                              | 4.27E+05                              | 4.26E+05                              |
| ADP fossil (MJ)                    | 3.44E+12      | 3.39E+12                              | 3.40E+12                              | 3.42E+12                              |
| FAETP (kgDCB <sub>eq</sub> )       | 7.43E+10      | 7.48E+10                              | 7.46E+10                              | 7.44E+10                              |
| HTP inf (kgDCB <sub>eq</sub> )     | 5.27E+10      | 5.25E+10                              | 5.26E+10                              | 5.26E+10                              |
| MAETP (kgDCB <sub>eq</sub> )       | 4.54E+14      | 4.54E+14                              | 4.54E+14                              | 4.54E+14                              |
| POCP (kgethene <sub>eq</sub> )     | 1.84E+08      | 1.84E+08                              | 1.84E+08                              | 1.84E+08                              |
| TETP (kgDCB <sub>eq</sub> )        | 1.49E+09      | 1.48E+09                              | 1.49E+09                              | 1.49E+09                              |

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1117 **2.2 CCUS of Italy**

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1119 Table S13 Results of sensitivity analysis for the CCUS of Italy

|                                    | Base case (A) | 25% CO <sub>2</sub> stored compared A | 50% CO <sub>2</sub> stored compared A | 75% CO <sub>2</sub> stored compared A |
|------------------------------------|---------------|---------------------------------------|---------------------------------------|---------------------------------------|
| GWP (kgCO <sub>2eq</sub> )         | 9.62E+10      | 9.24E+10                              | 9.39E+10                              | 9.48E+10                              |
| AP (kgSO <sub>2eq</sub> )          | 4.67E+08      | 4.62E+08                              | 4.64E+08                              | 4.65E+08                              |
| EP (kgPhosphate <sub>eq</sub> )    | 1.15E+11      | 1.15E+11                              | 1.15E+11                              | 1.15E+11                              |
| ODP (kgR11 <sub>eq</sub> )         | 3.68E+02      | 3.41E+02                              | 3.51E+02                              | 3.59E+02                              |
| ADP elements (kgSb <sub>eq</sub> ) | 2.27E+04      | 2.23E+04                              | 2.24E+04                              | 2.26E+04                              |
| ADP fossil (MJ)                    | 1.96E+12      | 1.91E+12                              | 1.93E+12                              | 1.94E+12                              |
| FAETP (kgDCB <sub>eq</sub> )       | 9.27E+10      | 9.17E+10                              | 9.21E+10                              | 9.22E+10                              |
| MAETP (kgDCB <sub>eq</sub> )       | 1.02E+13      | 9.64E+12                              | 9.84E+12                              | 1.00E+13                              |
| POCP (kgethene <sub>eq</sub> )     | 7.88E+07      | 7.78E+07                              | 7.82E+07                              | 7.84E+07                              |
| TETP (kgDCB <sub>eq</sub> )        | 4.42E+07      | 4.08E+07                              | 4.19E+07                              | 4.30E+07                              |

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### 1128 **3. Description of processes for CO<sub>2</sub> utilization**

#### 1129 3.1 Concrete curing

1130 In the concrete curing process, carbon dioxide is injected into the curing vessels at room temperature and here  
1131 diffuses into the fresh concrete under low pressure to produce calcium carbonate (CaCO<sub>3</sub>). In this reaction,  
1132 carbon dioxide reacts with cement components or hydration products such as 3CaO·SiO<sub>2</sub>, 2CaO·SiO<sub>2</sub>,  
1133 Ca(OH)<sub>2</sub>, xCaO·SiO<sub>2</sub>·yH<sub>2</sub>O gel etc (Thomas Concrete, 2018; Xuang et al., 2018). After a few hours, the so  
1134 obtained concrete has a higher compressive strength, better abrasion resistance, lower drying shrinkage and  
1135 costs due to a reduction of cement content than in conventional concrete (Shi-Cong et al., 2014).

#### 1136 3.2 Wheat production

1137 Carbon dioxide influences the photosynthesis, improving it because of its higher concentration in the  
1138 surrounding atmosphere. However, an excess of carbon dioxide alters carbon (C) and nitrogen (N) metabolism,  
1139 changing the chemical composition of agricultural plants (Hogy et al., 2009). This could determine higher  
1140 yield but lower quality. the results of free air concentration enrichment (FACE) tests are sometimes  
1141 contradicting the laboratory experiments about the quality (regarding the nitrogen and protein content) of the  
1142 agricultural products (Nuttall et al. 2017; Verrillo et al., 2017). Generally, it is recommended to keep carbon  
1143 dioxide concentration level just above that in the atmosphere in the growing environment where wheat is  
1144 cultivated on large scale (Watson et al., 2018, Erda et al. doi:10.1098/rstb.2005.1743).

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#### 1146 3.3 Lignin treatment

1147 Lignin is obtained through the extraction of black liquor, from the pulp mill industry. In this condition, it is  
1148 characterized by a pH between 13-14. However, to be used as raw material, a pH of about 8 should be achieved  
1149 treating lignin with carbon dioxide (Patricio et al., 2017). The treated lignin can be used as an additive for  
1150 concrete mixtures (Yufang et al., 2016), catalysts (Atul et al., 2013), polyethylene (Samal et al., 2014),  
1151 propylene (Gregorová et al., 2005) and other chemicals.

#### 1152 3.4 Polyurethane production

1153 Polyurethane is obtained in a conventional way by polyol and isocyanate through a catalytic reaction (von der  
1154 Assen et al., 2015). These two reagents are petroleum derived products. However, an alternative to this  
1155 conventional route is taken into account producing polyol from carbon dioxide. CO<sub>2</sub> reacts with epoxides to  
1156 produce polycarbonate polyols via a catalytic reaction (Orgilés-Calpena et al., 2016). The mechanical  
1157 properties of polyurethane are comparable with those obtained through a traditional way (Orgilés-Calpena et  
1158 al., 2016).

#### 1159 3.5 Calcium carbonate production via mineral carbonation

1160 Calcium carbonate is naturally produced and it is known as ground calcium carbonate (GCC). However, it can  
1161 be industrially produced via precipitation and it is known as precipitated calcium carbonate (PCC). In this  
1162 second route, steel slags are used as raw material that reacts with carbon dioxide to produce calcium carbonate  
1163 (Lee et al., 2016). In fact, steel slags are mainly composed by CaO and MgO in addition to heavy metals as  
1164 Mn, V, Zn, Cu, Ni, Cd, Pb, Sb, Mo, and Cr (Yadav and Mehra, 2017). An advantage of this process is that it  
1165 can be controlled to have the desired quality, purity and size of crystals (Eloneva et al., 2008).

### 1166 3.6 Urea production

1167 Urea is obtained from the reaction of ammonia and carbon dioxide. Ammonia is produced by the reaction of  
1168 hydrogen and nitrogen, where the first one is obtained by syngas obtained from natural gas reforming. In  
1169 particular, two different steps are involved: at first ammonium carbamate is obtained in the liquid state while  
1170 in the second step urea is formed by dehydrogenation of ammonium carbamate. Different process schemes are  
1171 proposed by Koohestanian et al. (2018) and Edrisi et al. (2013, 2014a, 2014b, 2016).

### 1172 3.7 Methanol production

1173 A traditional way to produce methanol is the indirect way, via syngas hydrogenation, where syngas is obtained  
1174 by the steam reforming of natural gas (Olah et al., 2005). A more environmentally friendly way is according  
1175 to the catalytic direct hydrogenation of carbon dioxide using CuO/ZnO/Al<sub>2</sub>O<sub>3</sub> as catalyst (Leonzio, 2018).  
1176 Hydrogen can be obtained from the electrolysis of water exploiting renewable energies (solar or wind  
1177 energies), from biomass pyrolysis, coke oven gas, reforming of biomass-derived products or partial oxidation  
1178 of light oil residues (Leonzio, 2018). The hydrogenation of carbon dioxide is kinetically and  
1179 thermodynamically limited then the recycle of unconverted gases after the separation of methanol and water,  
1180 the utilization of membrane permeable to water are solutions that can be considered to improve conversions  
1181 and yields (Leonzio et al., 2019).

### 1182 3.8 Concrete by red mud production

1183 Red mud, known also as “bauxite residue”, is obtained by bauxite treatment in the alumina production. It is  
1184 characterized by an high value of pH (between 10.5-12.5) due to the presence of Al<sub>2</sub>O<sub>3</sub>, Fe<sub>2</sub>O<sub>3</sub>, SiO<sub>2</sub>, TiO<sub>2</sub>,  
1185 CaO, Na<sub>2</sub>O, then it is disposed in landfills (Patricio et al., 2017). A way to reduce the pH and use it as a raw  
1186 material consists on treating red mud with carbon dioxide. Generally, the treated read mud can be used as  
1187 additive for building materials, as adsorbent for the removal of heavy metals, for the preparation of catalysts,  
1188 ceramics, pigments, polymers and paints, for the recovery of iron, aluminum, titanium (Sutar et al., 2014; Liu  
1189 et al., 2009). It is found that corrosion resistance, compressive strength, elasticity modulus, splitting tensile  
1190 strength can be improved if concrete is composed by about 20% wt of red mud (Ribeiro et al., 2012; Liu and  
1191 Poon, 2016).

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1194 3.9 Methane production

1195 Methane can be produced by hydrogenation of carbon dioxide via power to gas system (Leonzio, 2017). In  
1196 this case hydrogen is obtained via water electrolysis using fluctuant renewable energies. The hydrogenation  
1197 reaction is called Sabatier reaction: it is exothermic and is carried out in a range of temperature between 200 °C  
1198 and 500 °C and at relatively high pressure (10-30 bar) (Stangeland et al., 2015). A Nickel based catalyst is  
1199 used for this reaction, even if Ru, Rh and Co on various oxide supports (TiO<sub>2</sub>, SiO<sub>2</sub>, MgO, and Al<sub>2</sub>O<sub>3</sub>) can also  
1200 be used (Brooks et al., 2007; Kopyscinski et al., 2010). Adiabatic fixed bed methanation reactors, isothermal  
1201 fluidized bed reactors are used for this reaction (Di Felice and Micheli, 2015). The biological methanation can  
1202 be also considered for power to gas systems (Ma et al., 2018).

1203

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